

On Mixing and Shaking: Structure and Dynamics of Turbulent Stratified Flames

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S. Hochgreb



ECM 2013, Lund, 25-28, 2013



The two limits of flame combustion

diffusion



$$T_s = T_0 + Q/c_p Y_F^0 z_s$$

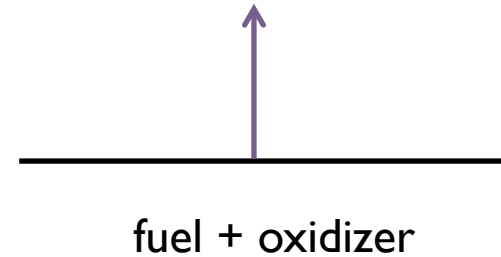
$$z_s = \frac{1}{1 + \phi^0}$$



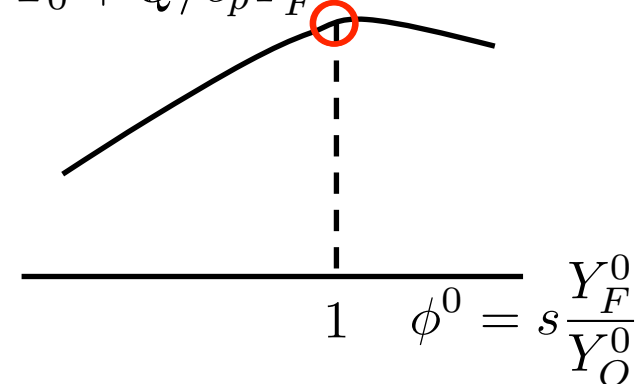
oxidizer z z_s fuel

High NO_x, Soot
Good dynamic range

premixed



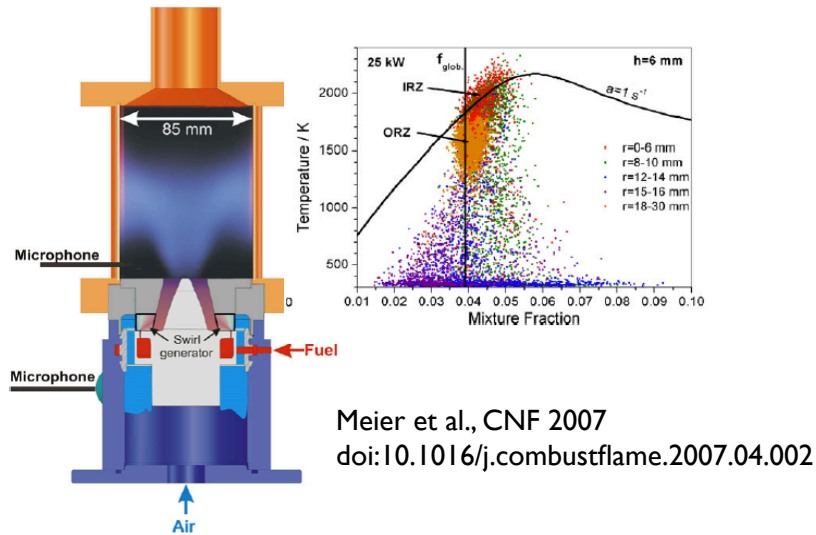
$$T_s = T_0 + Q/c_p Y_F^0$$



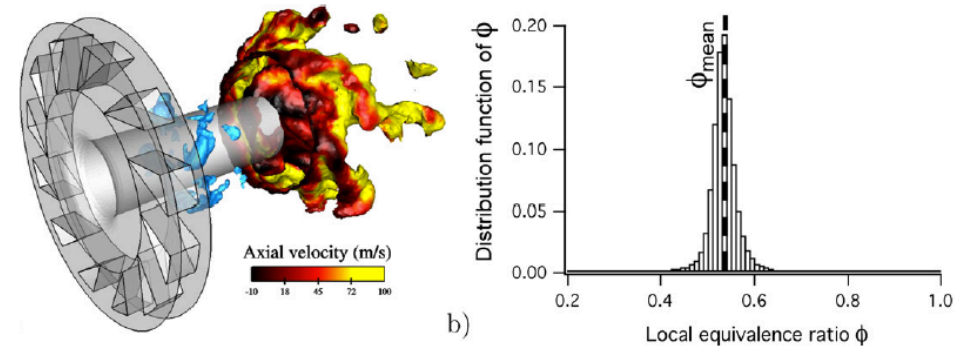
1 $\phi^0 = s \frac{Y_F^0}{Y_O^0}$

Low NO_x, soot, CO
Narrow dynamic range

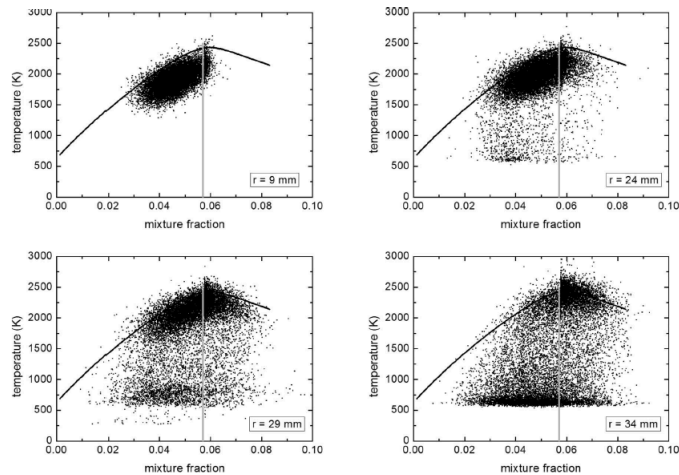
Stratified/technically premixed flames



Meier et al., CNF 2007
doi:10.1016/j.combustflame.2007.04.002

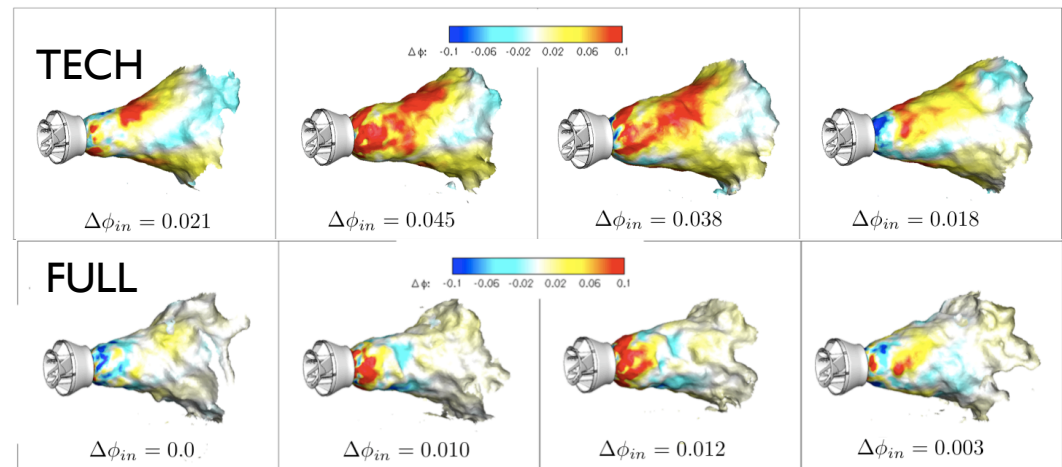


Sengissen et al, 2007
doi:10.1016/j.combustflame.2007.02.009



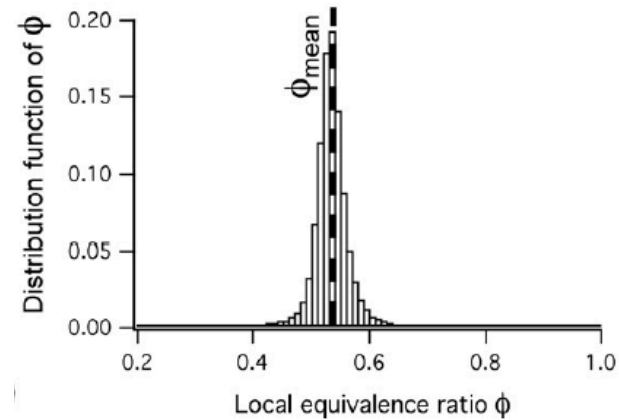
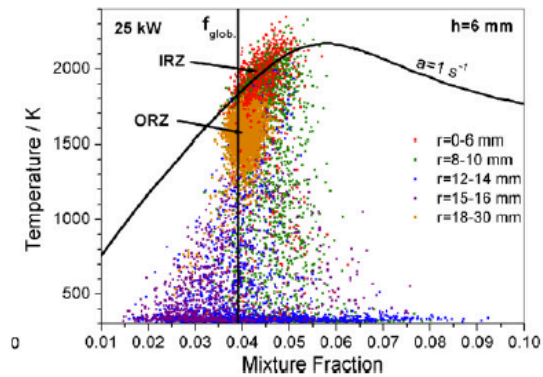
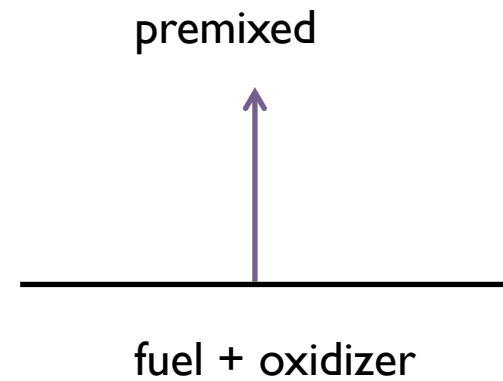
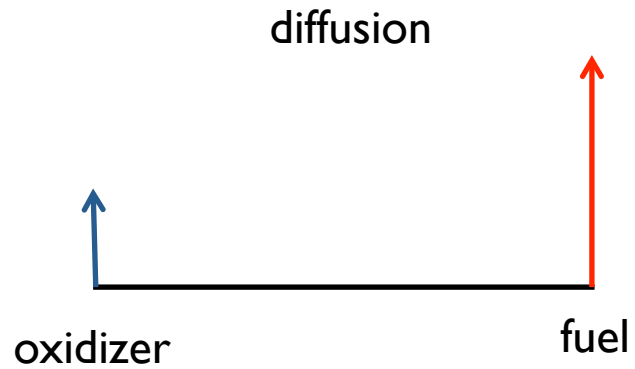
EV burner

Ax et al, JGTPP, 2010
doi: 10.1115/1.3205033



Hermeth et al, PCI 34 (2013)
doi: 10.1016/j.proci.2012.07.013

The two limits of flame combustion



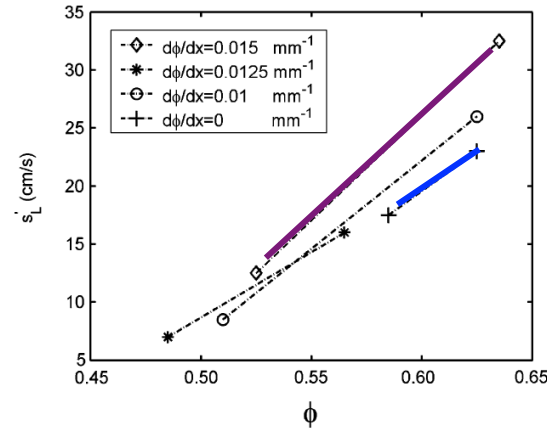
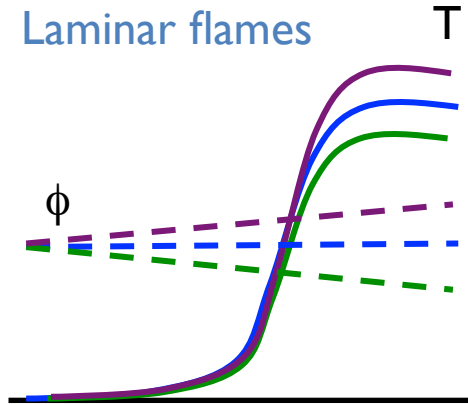
Meier et al., CNF 2007
 doi:10.1016/j.combustflame.2007.04.002

Ax et al., JGTTP, 2010
 doi: 10.1115/1.3205033

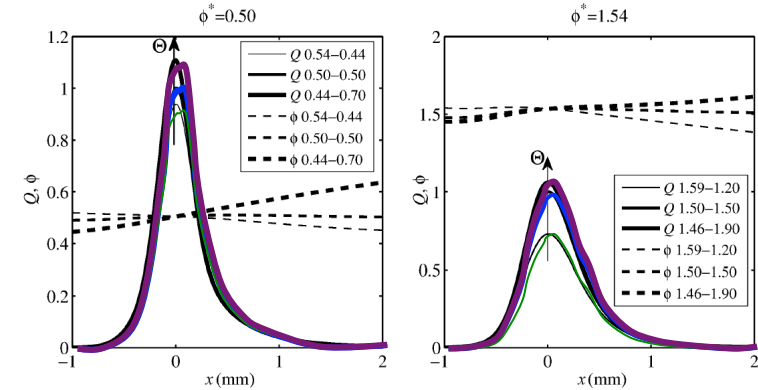
Are models for stratified flames adequate?

Why should we think stratified flames might be different?

Laminar flames

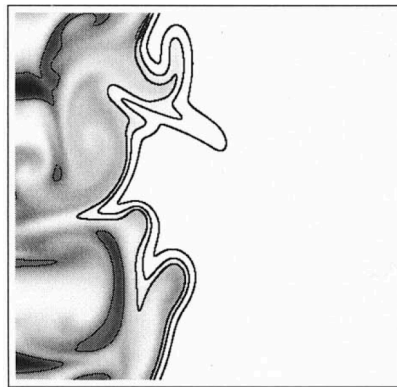


Kang & Kyritsis, CST, 177 (2005)
DOI: 10.1080/00102200500240836

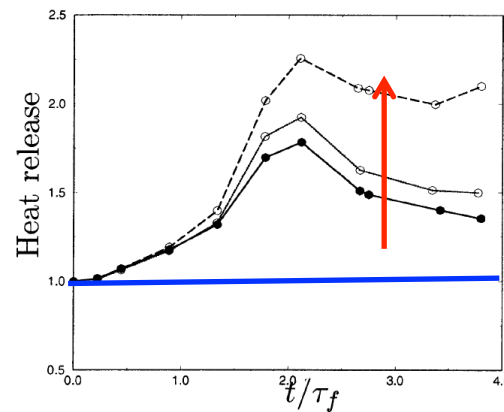


Zhou & Hochgreb, CNF, 160 (2013)
DOI: 10.1016/j.combustflame.2013.01.023

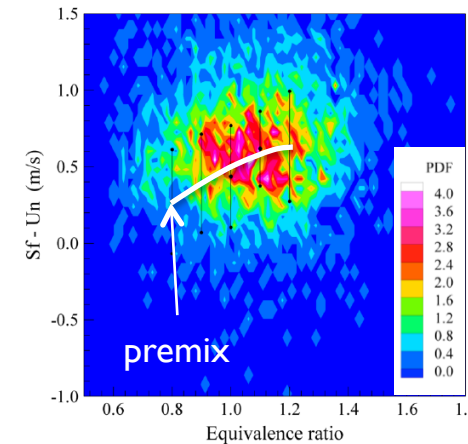
Turbulent flames



Propane mass fractions at $t/\tau_f = 4$



Jimenez et al, CNF 128:1-21 (2002)

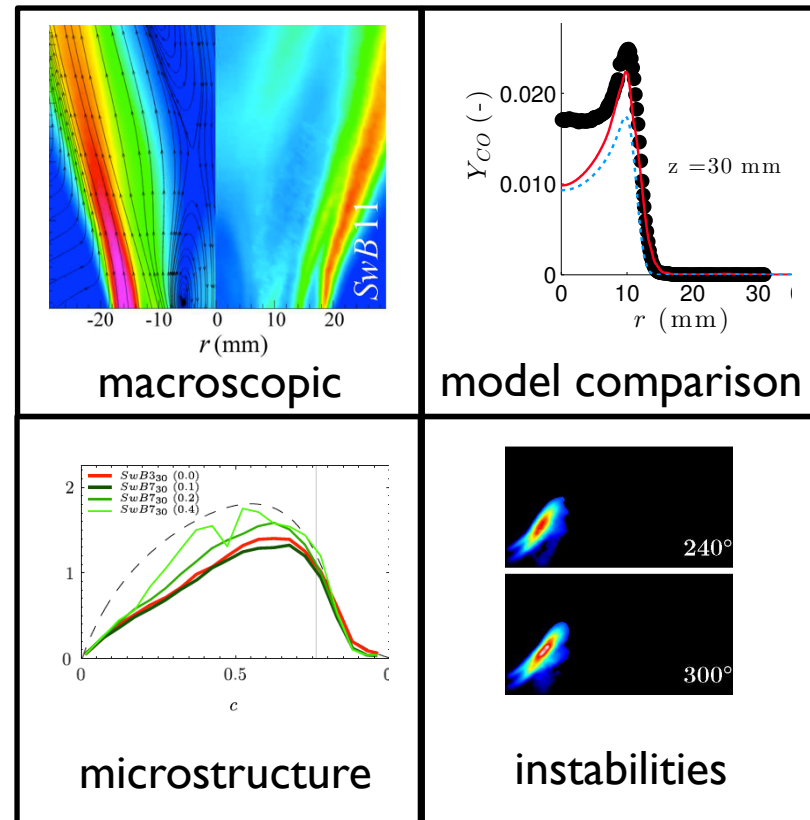


(b) $S_f - U_n$ vs. ϕ (1 ms)

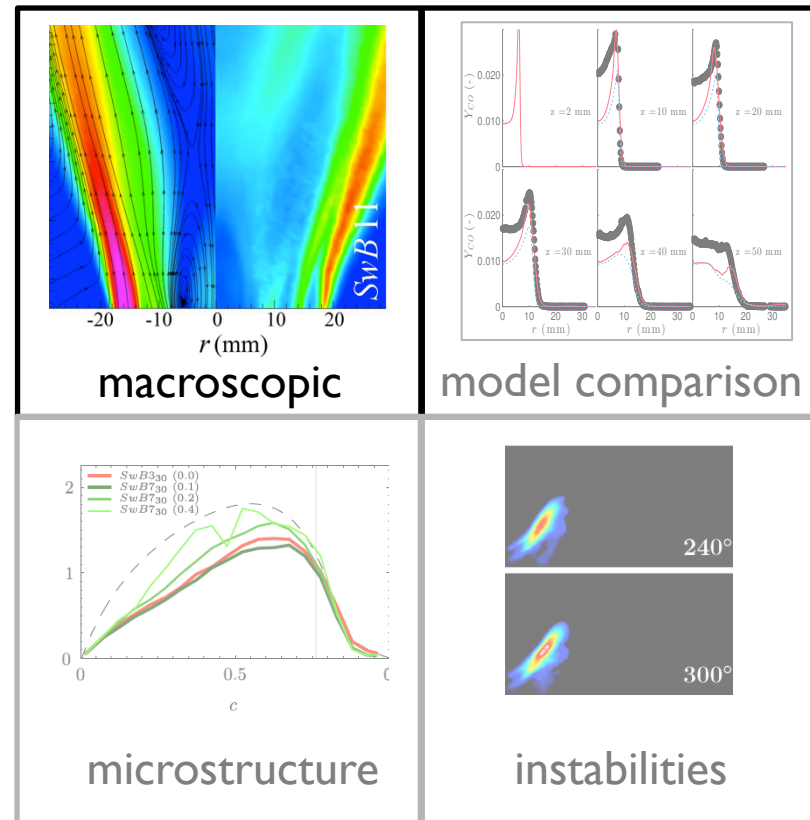
Pasquier, N. et al.,
PCI 31(2007) 1567-1574
Doi: 10.1016/j.proci.2006.07.118

Higher rates of heat release in lean flames for the same mean/local ϕ

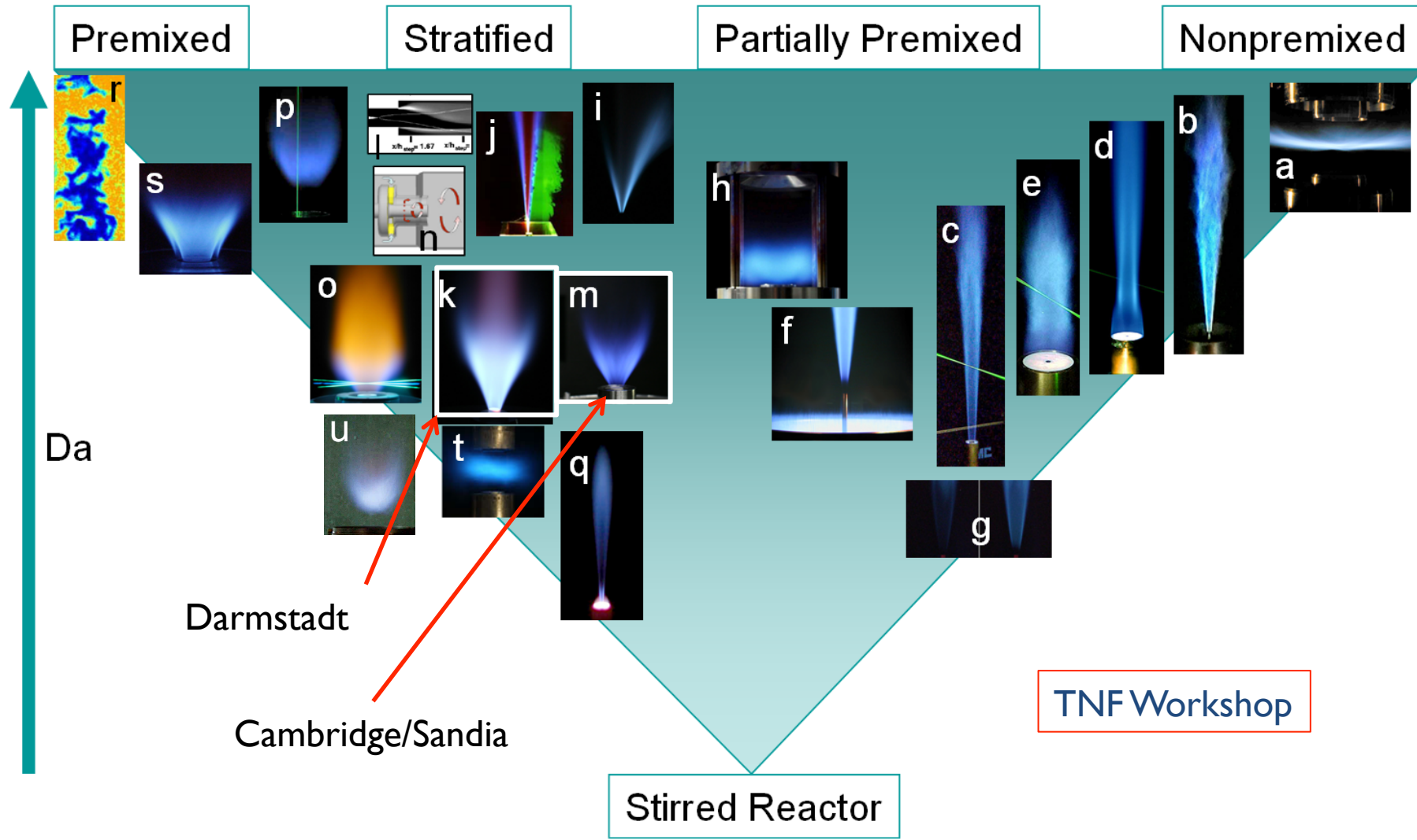
Outline: Effects of Stratification



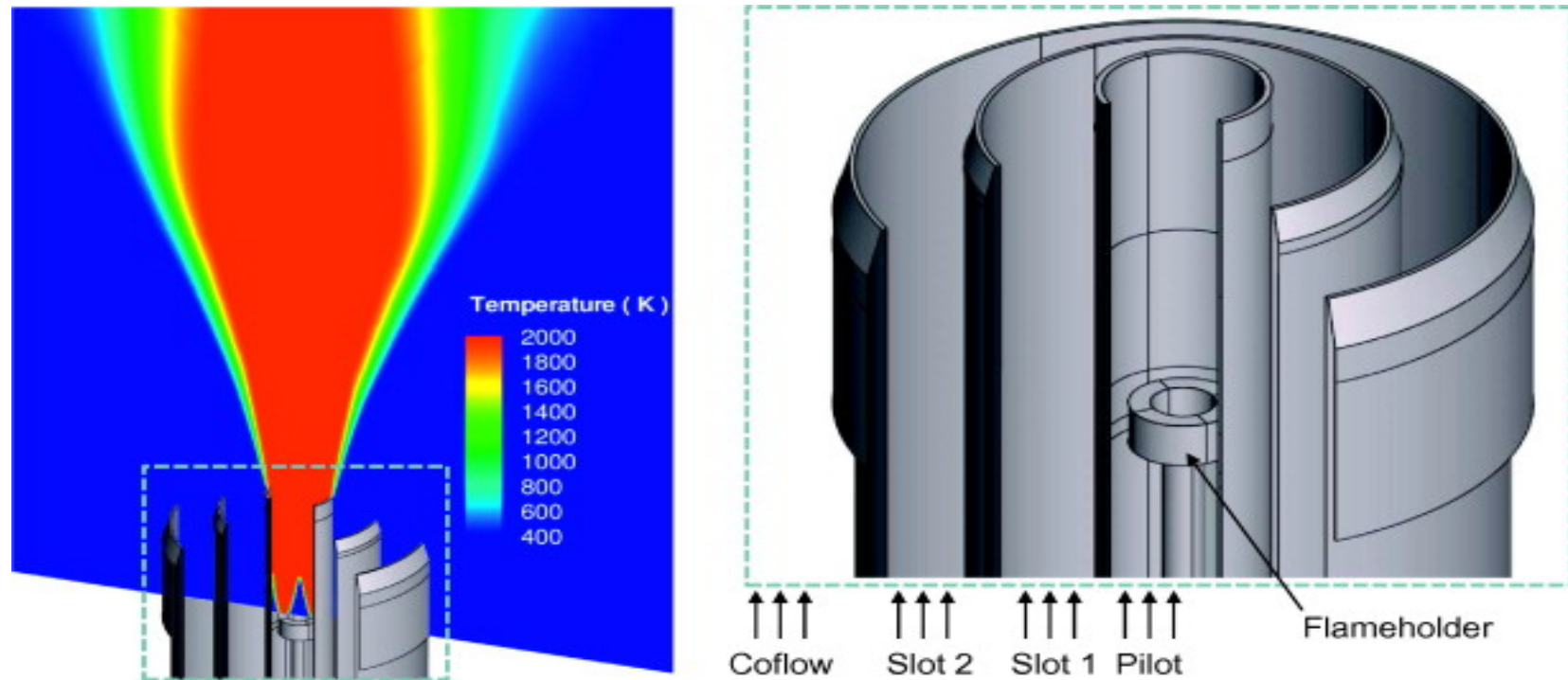
Outline: Effects of Stratification



Many contributors to the topic

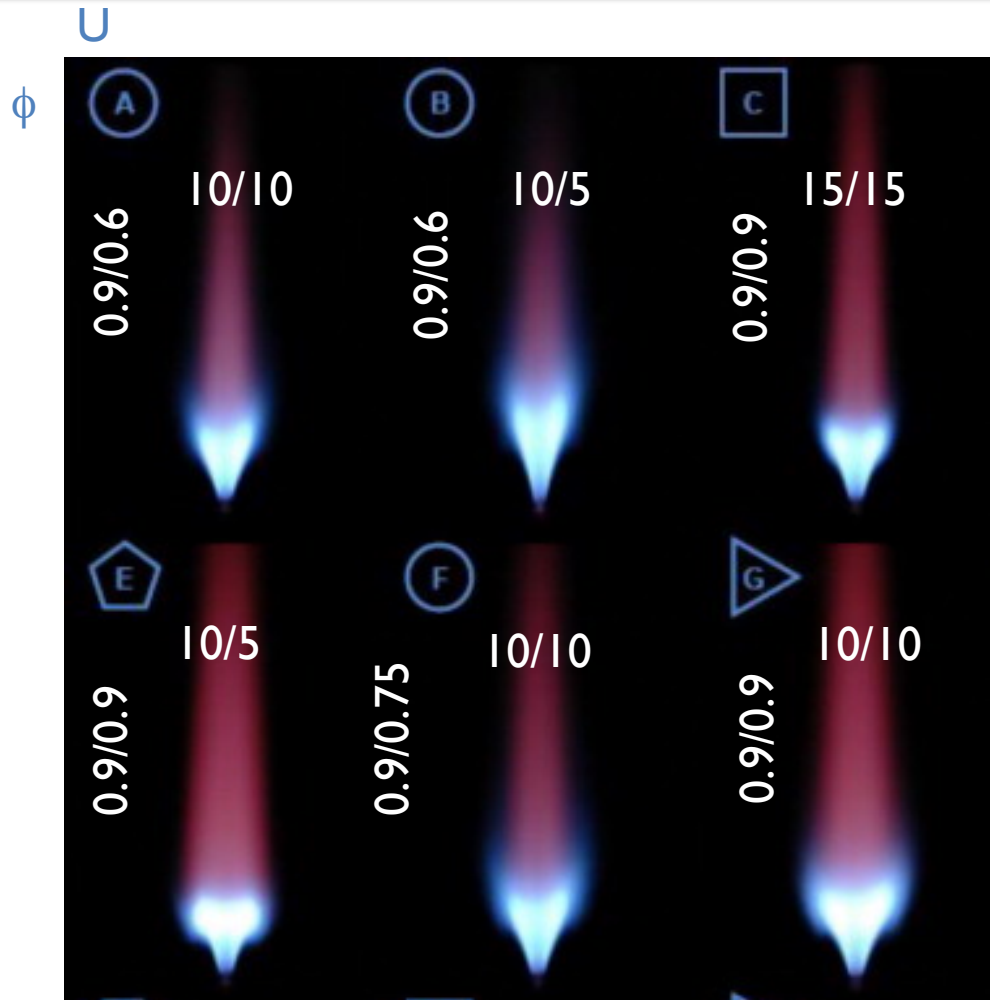


TUD Stratified Flame

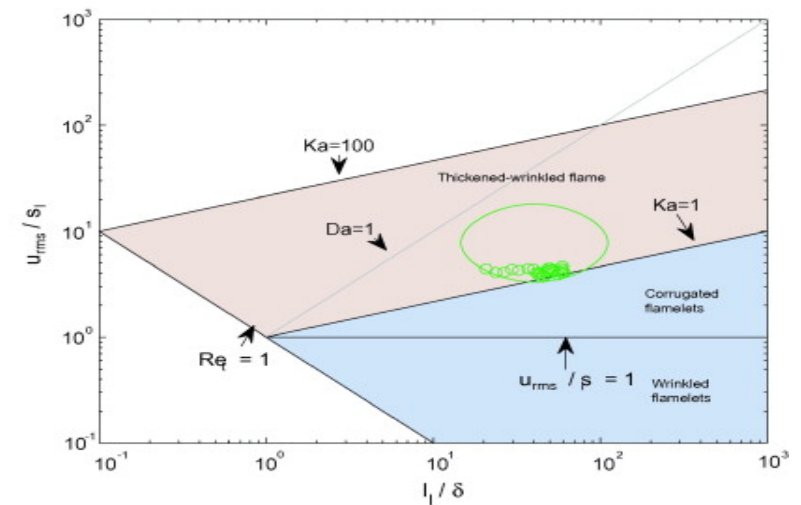


Seffrin et al, C&F157 (2010)
Boehm et al, PCI 33 (2011)
Kuenne et al, C&F 159 (2012), ECM (2013)

TUD Stratified Flame Properties

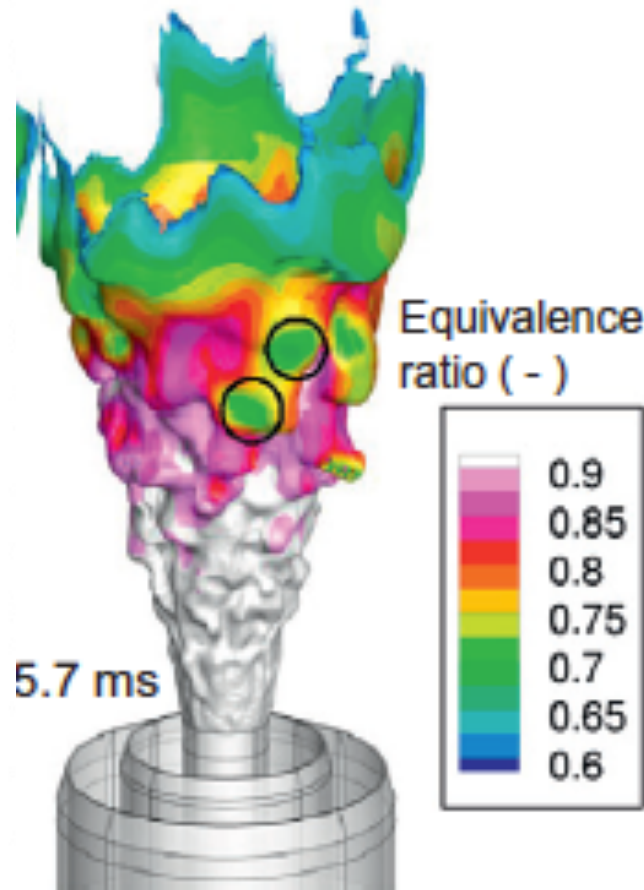
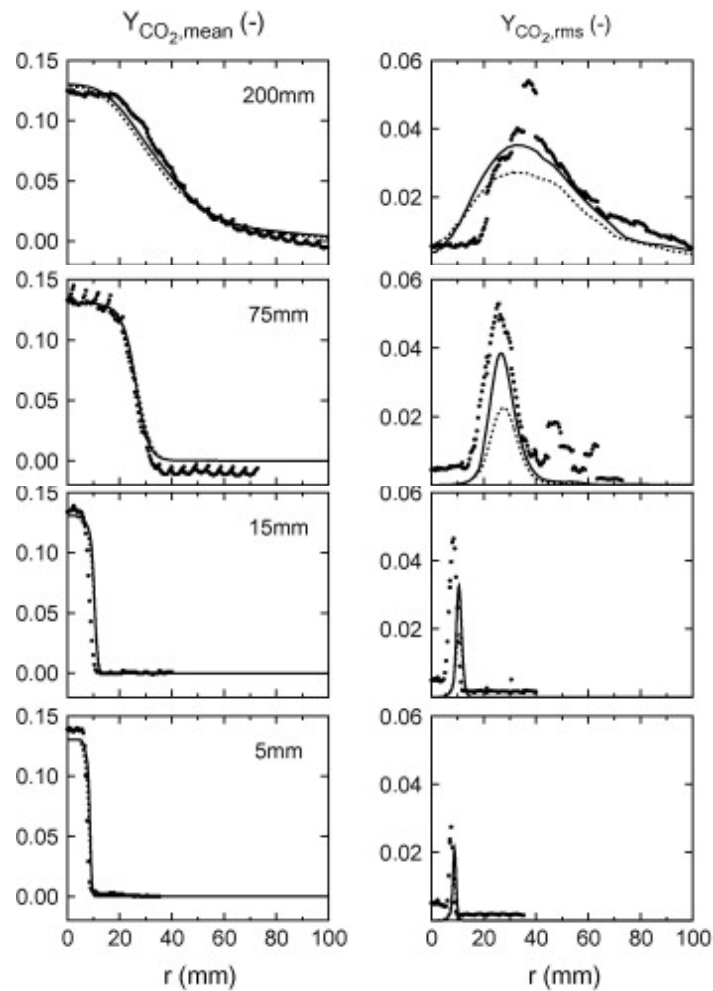


U (m/s)	5-20
u'/S_L (-)	0.35-0.9
Re_{hl}	13-26k
$Ka = (\delta_T/h)^2$	1.2-2.1
Da	50-80



Seffrin et al, CNFI57 (2010)

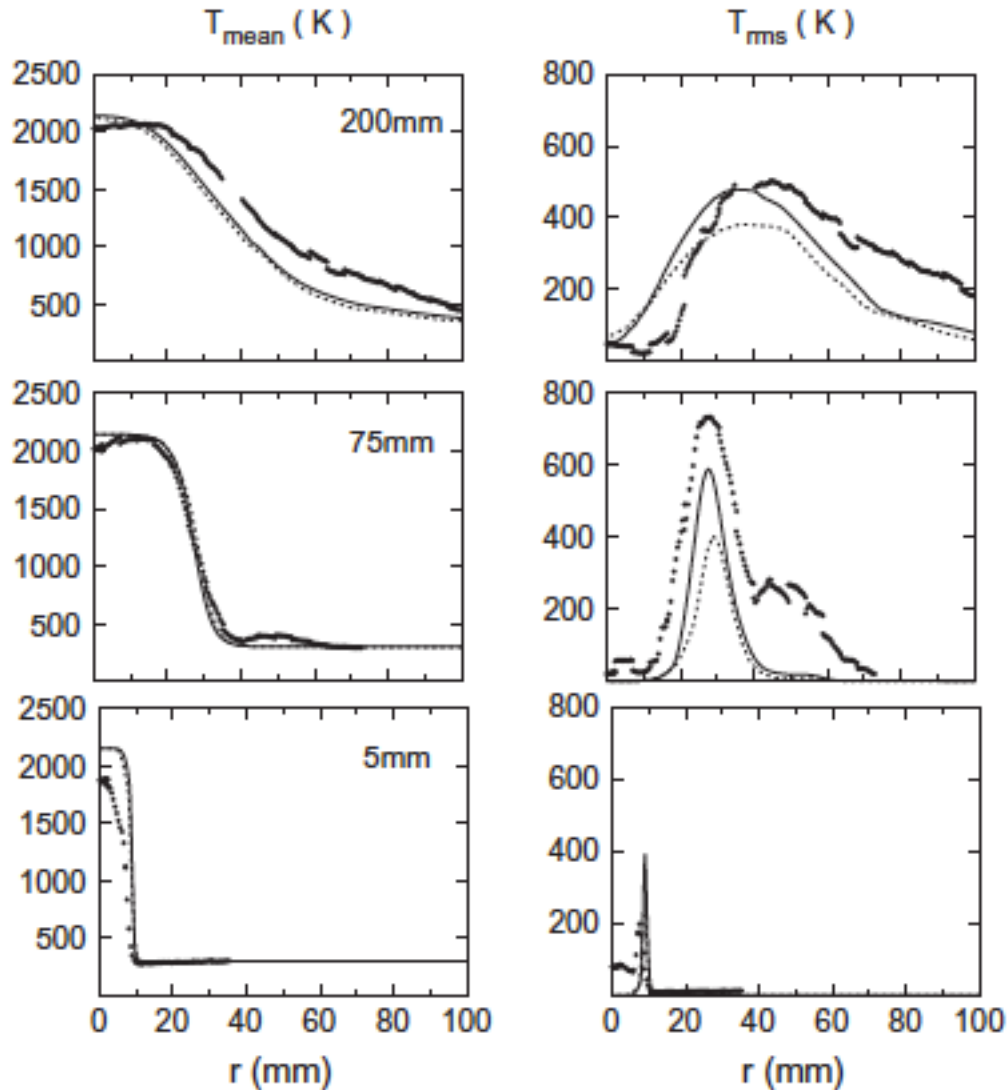
Comparison of model and experiment TUD stratified flame



FGM model
Thickened flame
Local cell ϕ

TSF-A-r
10 m/s no shear
 $\phi_i/\phi_o = 0.9/0.6$

Comparison of model and experiment – TUD stratified flame

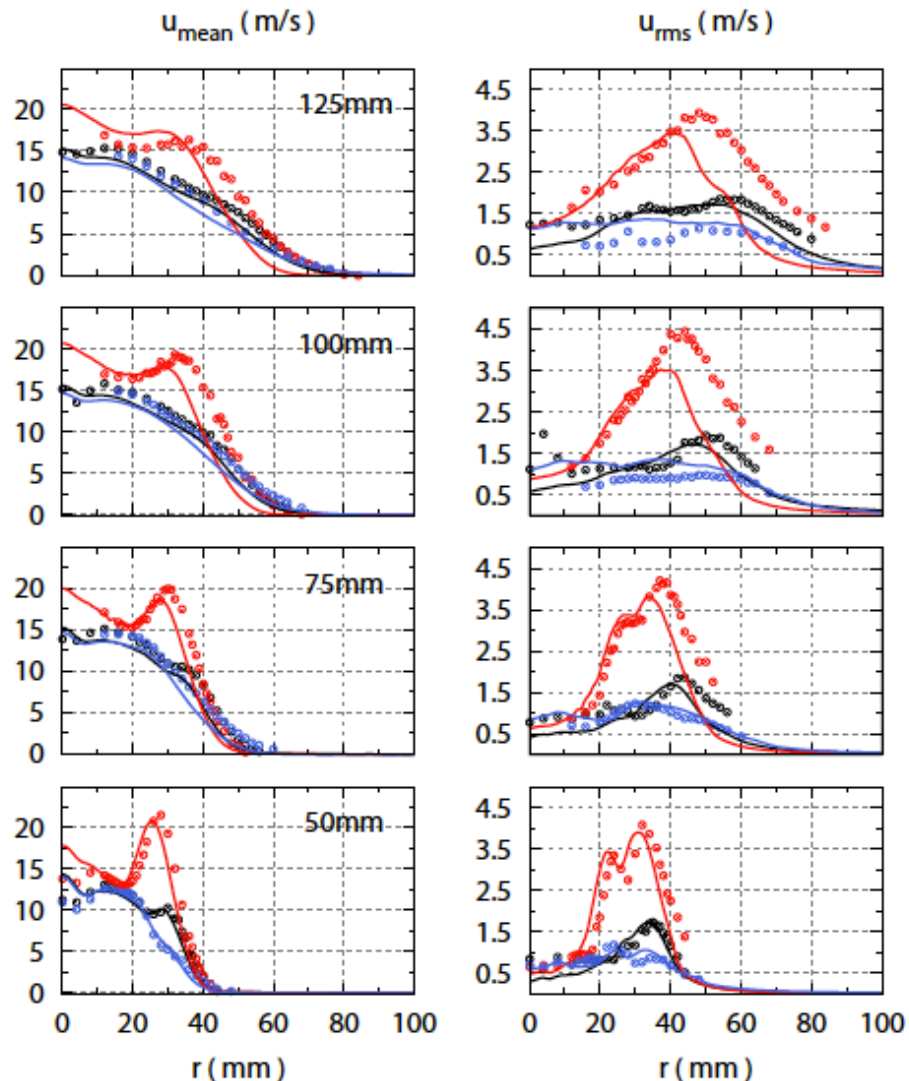


FGM model
Thickened flame
Local cell ϕ

TSF-A-r
10 m/s no shear
 $\phi_i/\phi_o = 0.9/0.6$

Velocity predictions and model

Shear cases



FGM model
Thickened flame
Local cell ϕ

U_i/U_o (m/s)

10/10

10/5

10/20

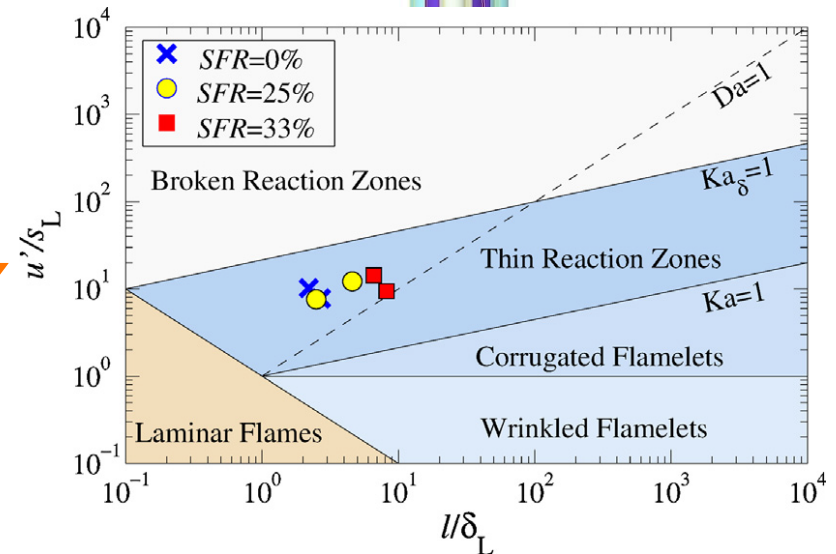
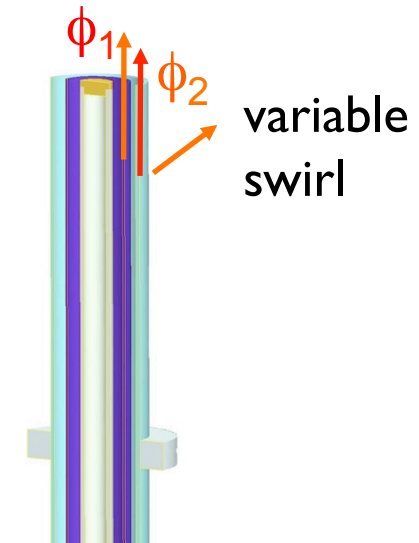
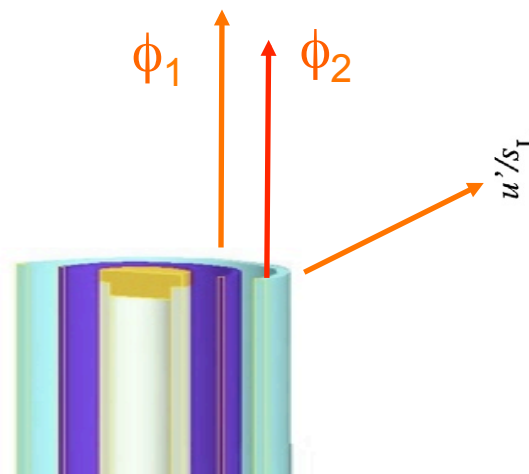
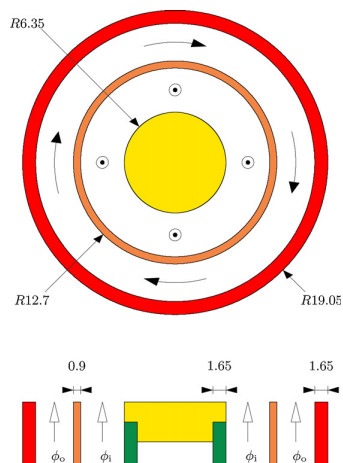
Kuenne et al., ECM 2013
Kuenne et al., CNF, 159 (2012)
doi:10.1016/j.combustflame.2012.02.010

More data and simulations underway

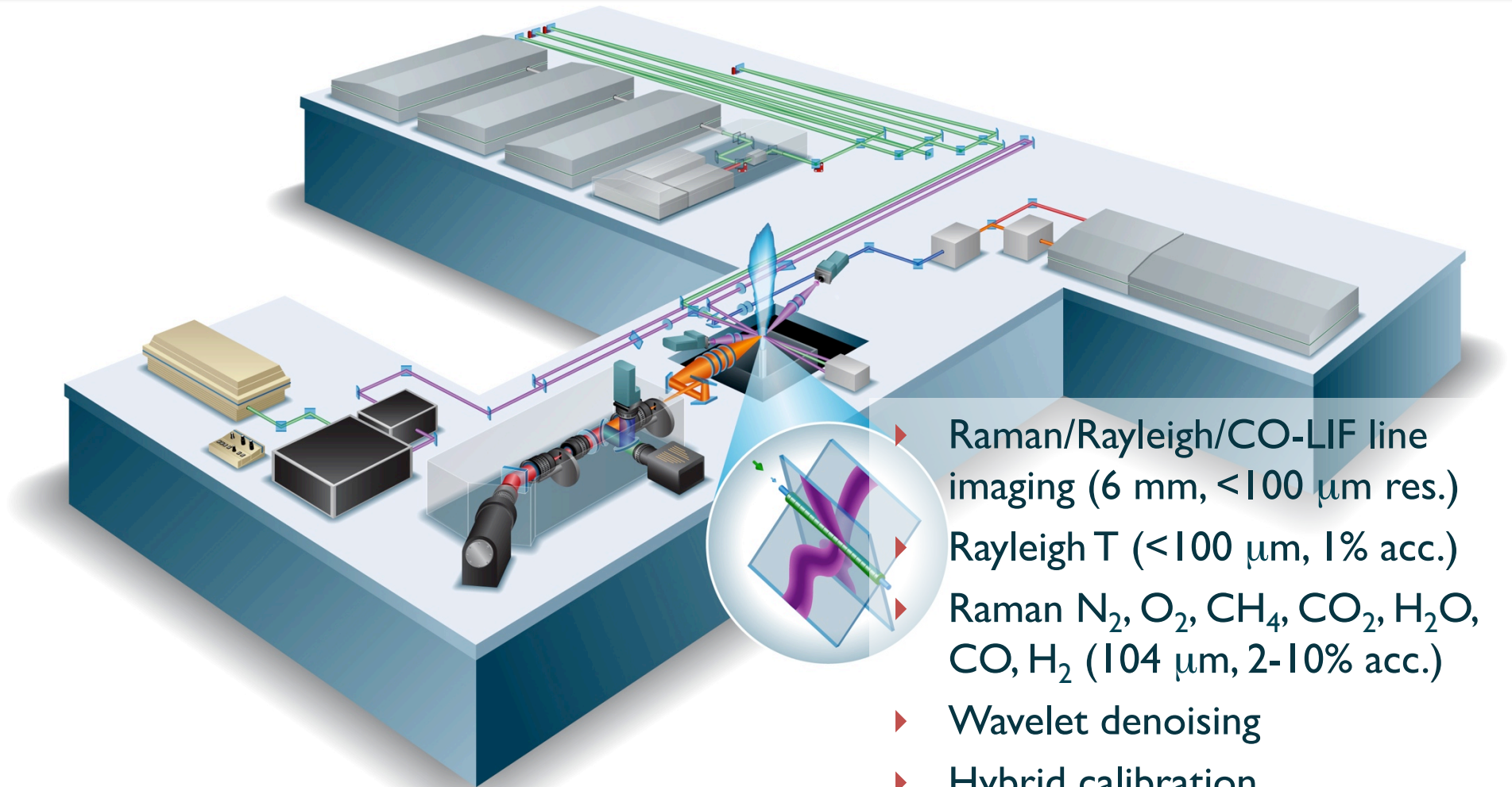
Sandia-Cambridge Stratified Swirl Burner

U_1 (m/s)	8.3	U_2 (m/s)	18.7
u'/U (-)	0.2-0.4	u'/S_L (-)	4-8
Re_{h1}	5690	Re_{h2}	11500
L_t (mm)	~9	Re_t	100-500
Da	0.6-1.0	$Ka = (\delta_T/\eta)^2$	7.6-48

Sweeney, Hochgreb, Dunn, Barlow
 C&F 159 (2012) 2896–2911
 C&F 159 (2012) 2912–2929
 C&F 160 (2013) 322-334
 C&F 33 (2011) 1419–1427

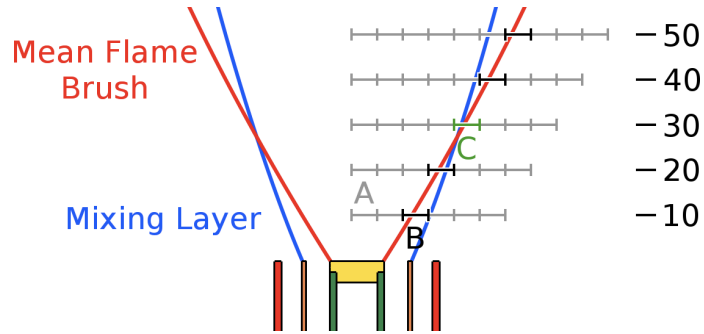


High resolution measurements: Sandia multiscalar facility



- ▶ Raman/Rayleigh/CO-LIF line imaging (6 mm, $<100 \mu\text{m}$ res.)
- ▶ Rayleigh T ($<100 \mu\text{m}$, 1% acc.)
- ▶ Raman N_2 , O_2 , CH_4 , CO_2 , H_2O , CO , H_2 ($104 \mu\text{m}$, 2-10% acc.)
- ▶ Wavelet denoising
- ▶ Hybrid calibration
- ▶ Crossed OH PLIF

Sandia-Cambridge Stratified Swirl Burner

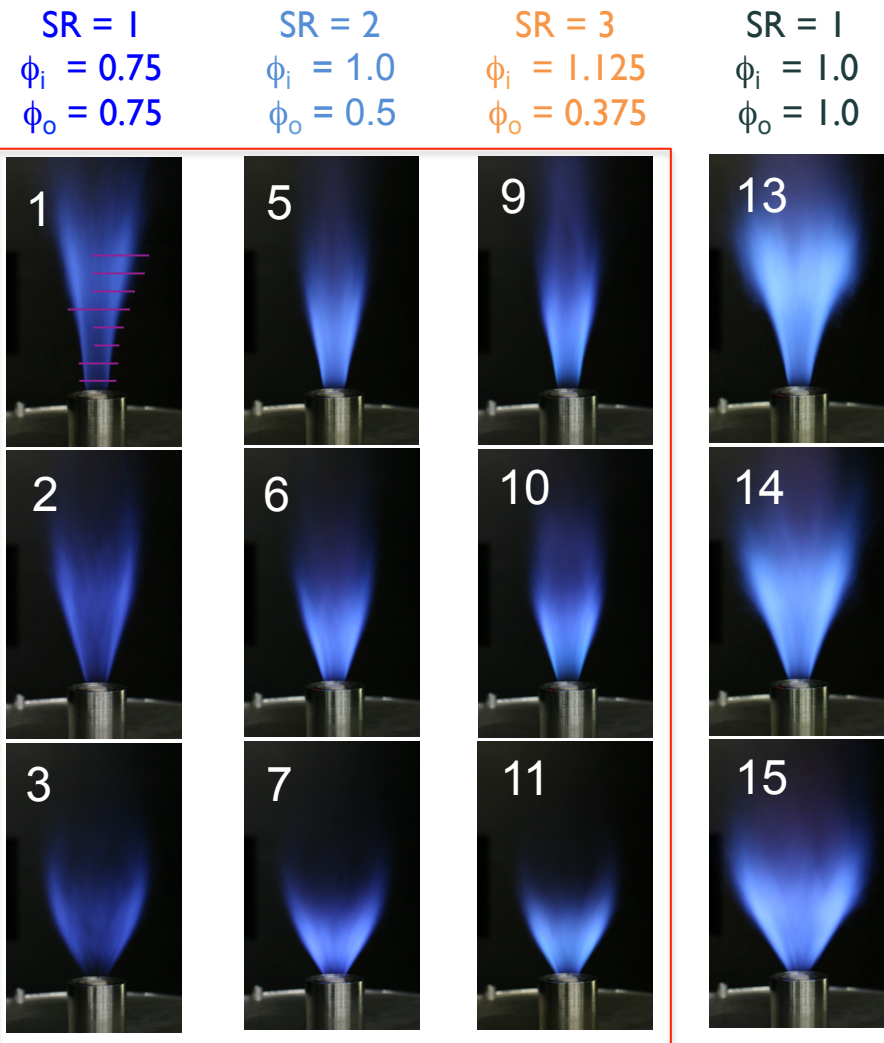


Radial profiles

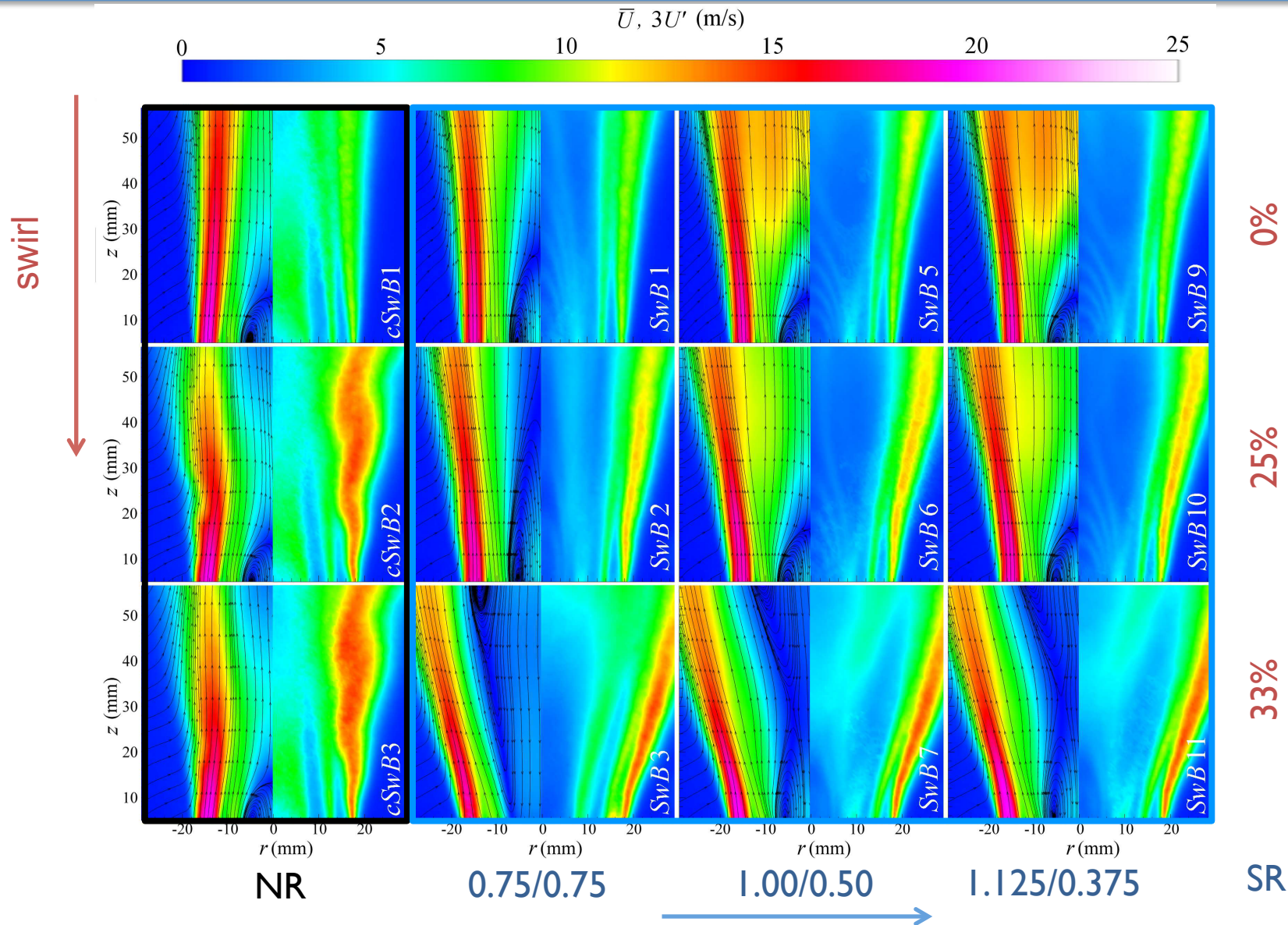
$z = 10, 20, 30, \dots, 80$ mm
 300 shots at each location,
 1500 in flame brush
 103 μm data spacing

Long records

crossing of flame & mixing layer
 30,000 shots
 20 μm data spacing
 wavelet denoising

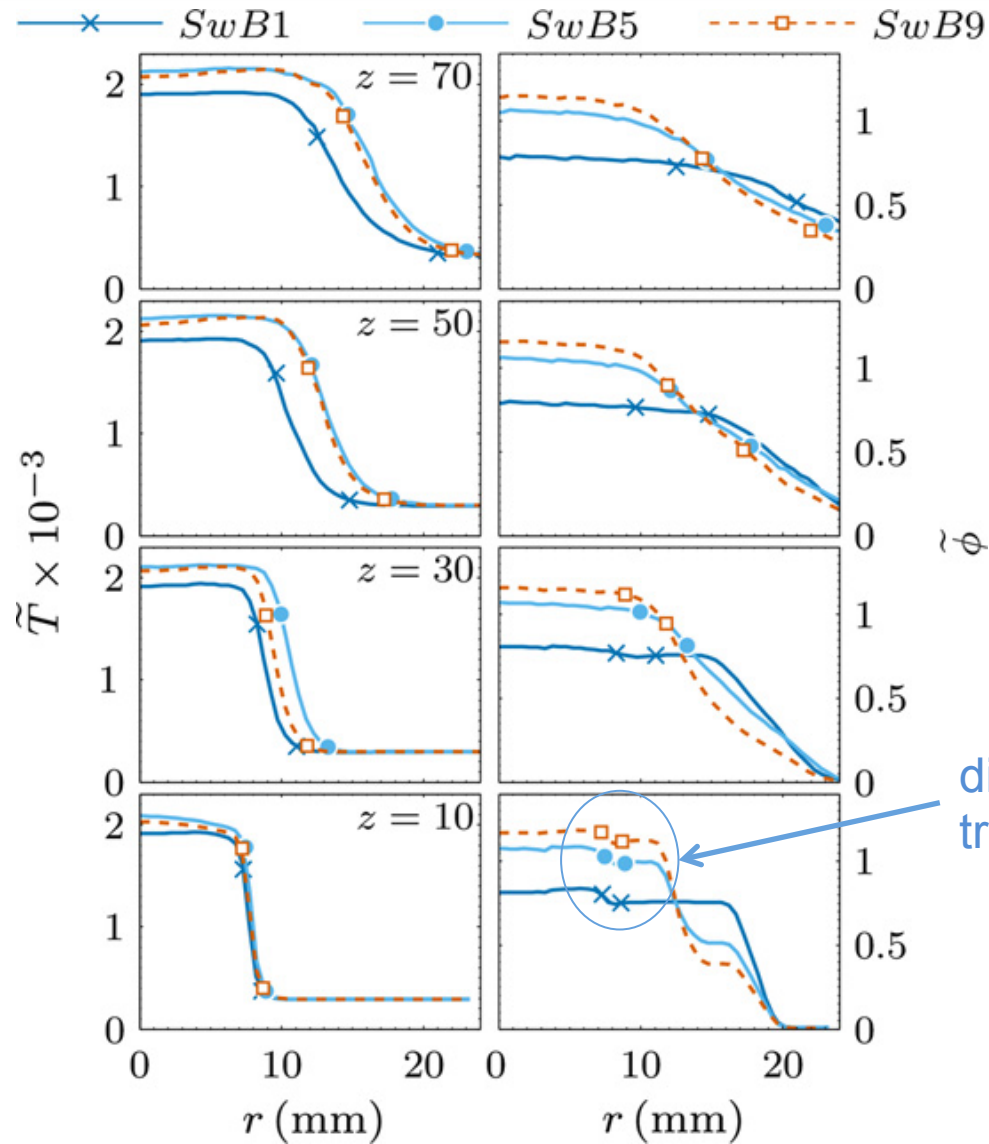


Mean velocity profiles: swirl and non-swirl



Zhou & hochgreb, CNF 2013,
doi: 10.1016/j.combustflame.2013.04.007

No swirl: Favre averaged \bar{T} and ϕ



SwB1: SR = 1.0

SwB5: SR = 2.0

SwB9: SR = 3.0

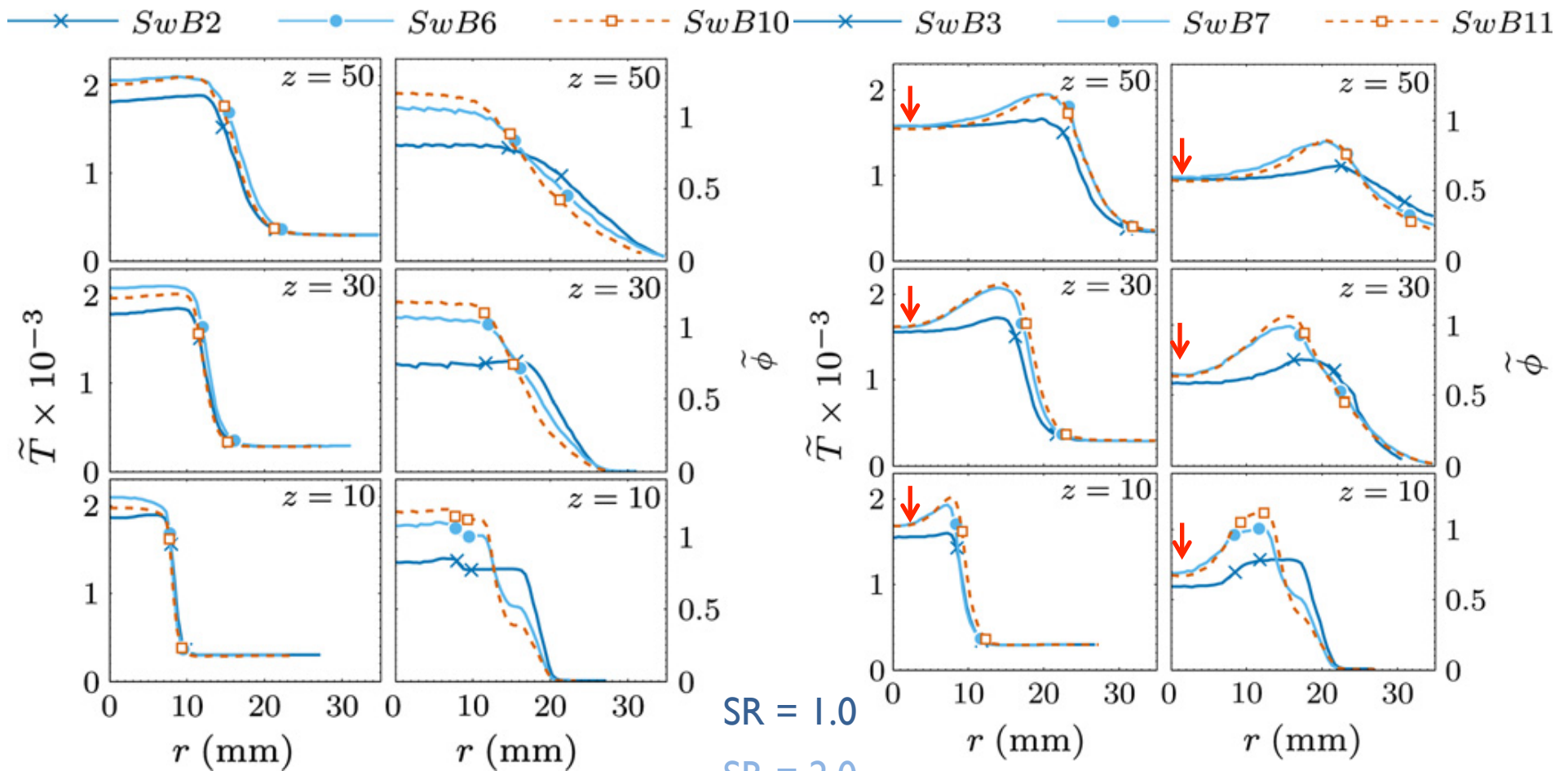
differential
transport

Sweeney et al, CNF 159 (2012)
doi:10.1016/j.combustflame.2012.06.001

Swirl: T and ϕ profiles

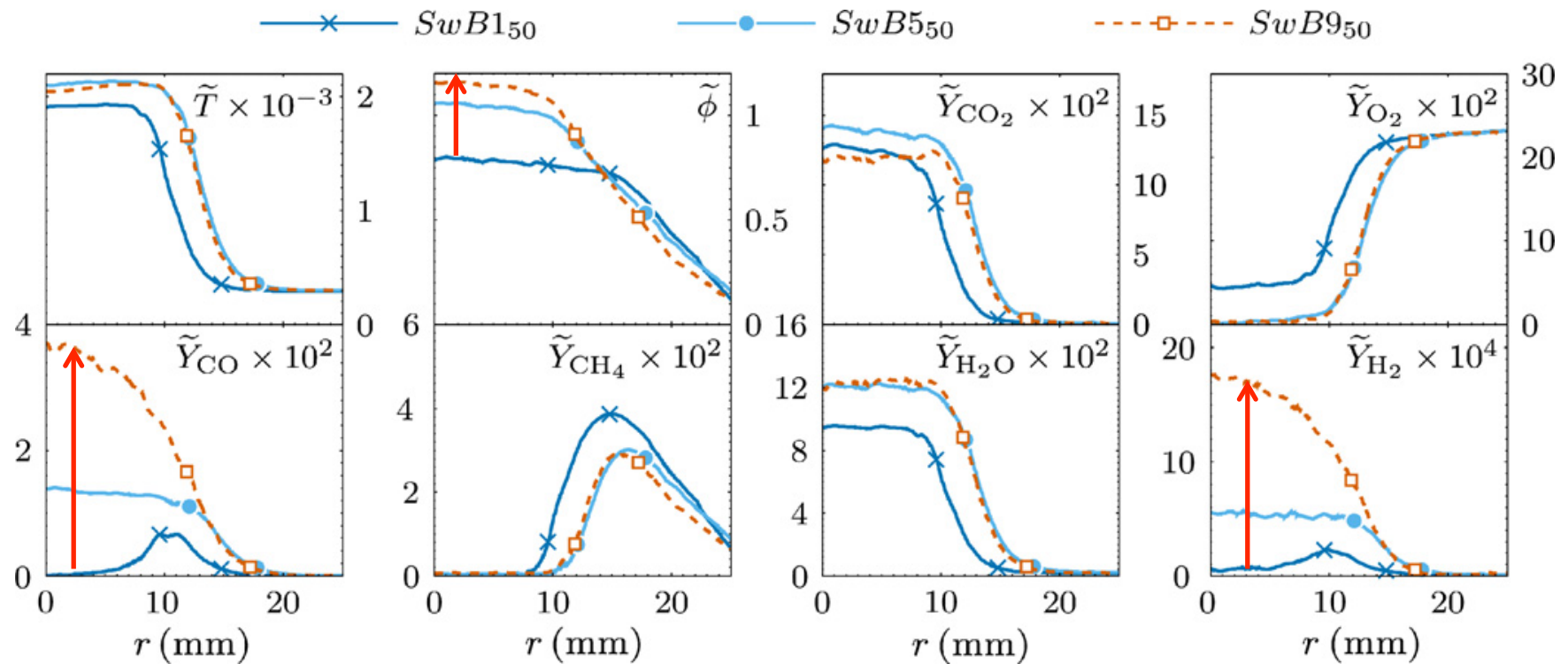
SFR = 0.25

SFR = 0.33



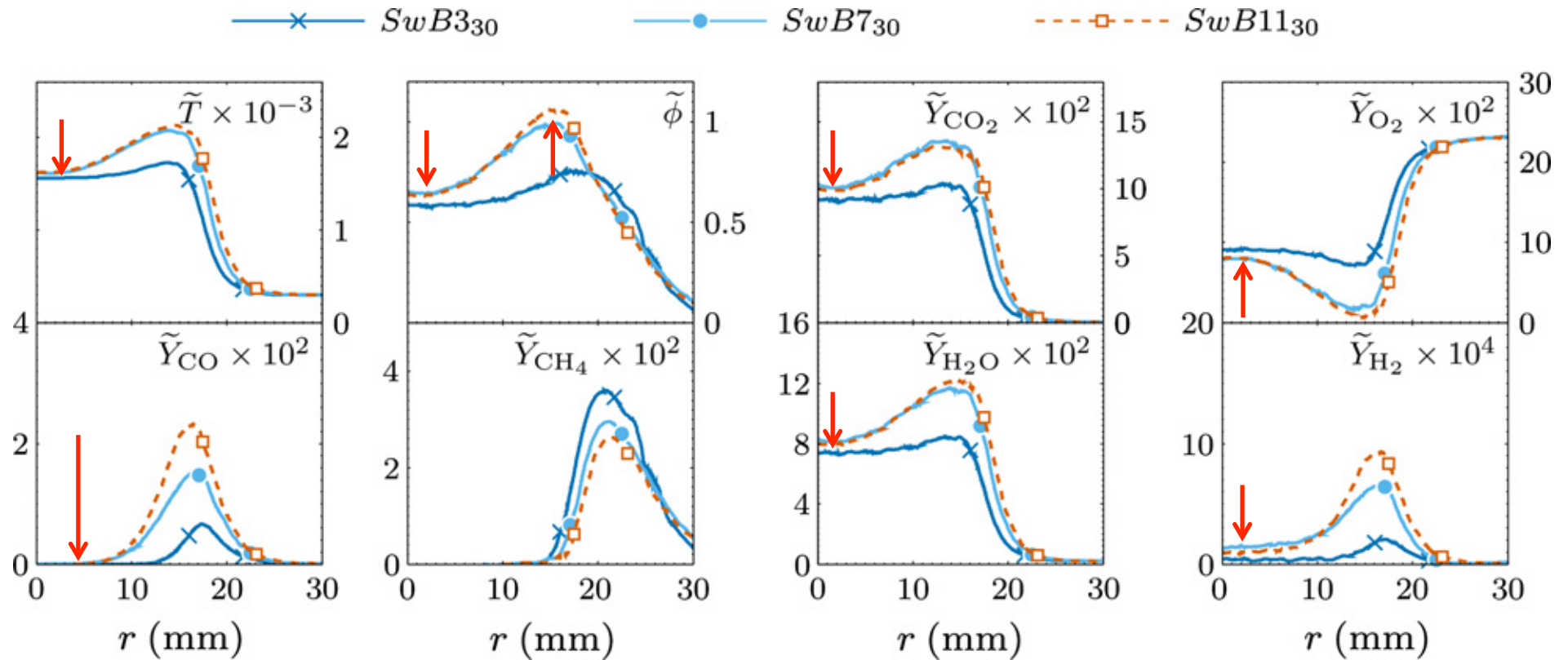
Sweeney et al, 159 (2012)
 doi:10.1016/j.combustflame.2012.05.014

No swirl: Favre species profiles

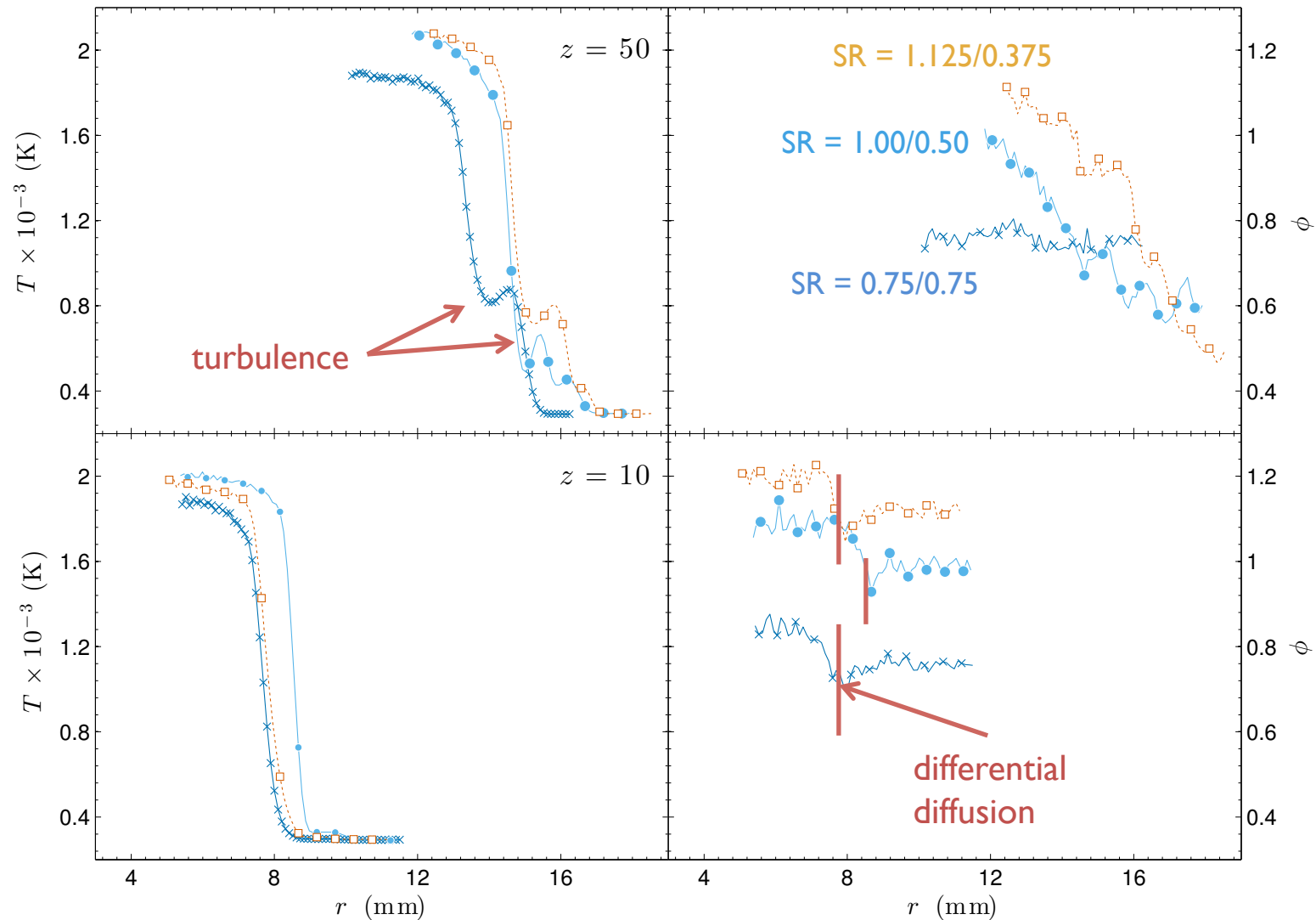


$z=50$ mm: approximate location of mixing layer crossing

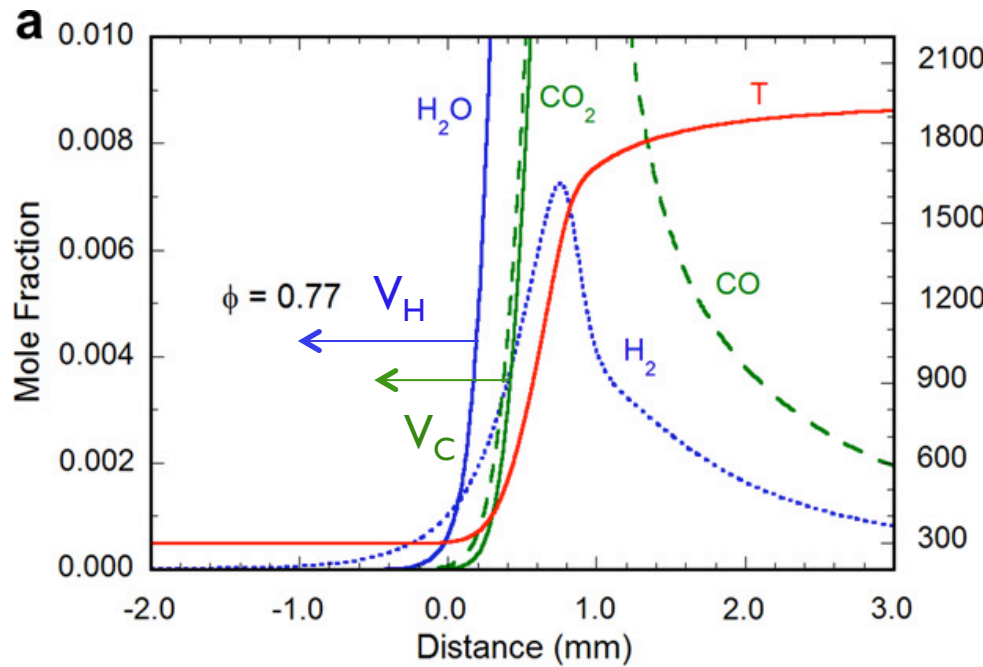
Swirl: Favre species profiles



The story of differential diffusion: Single shots



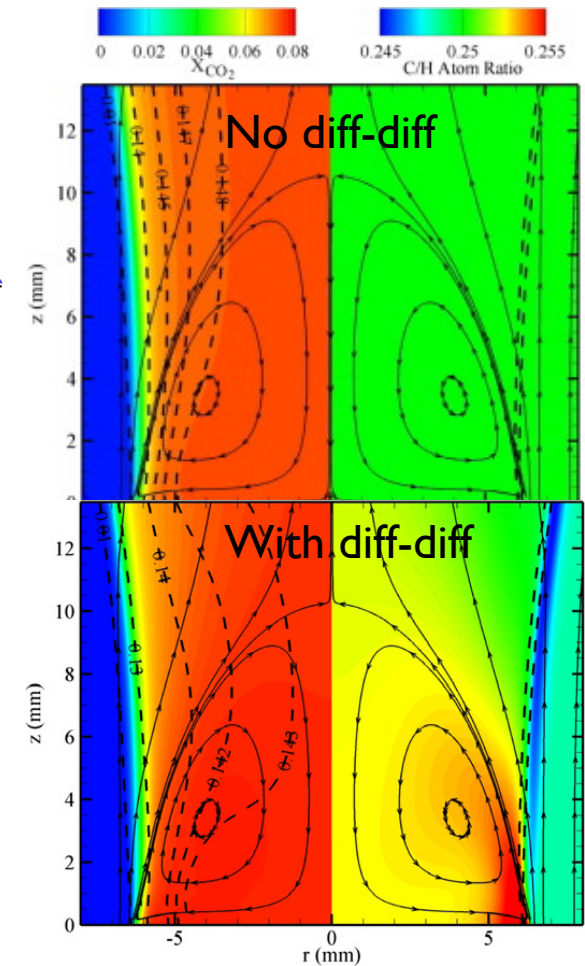
Mechanism for differential transport in bluff body stabilized burners



Barlow et al, C&F 159 (2012)
doi:10.1016/j.combustflame.2011.11.013

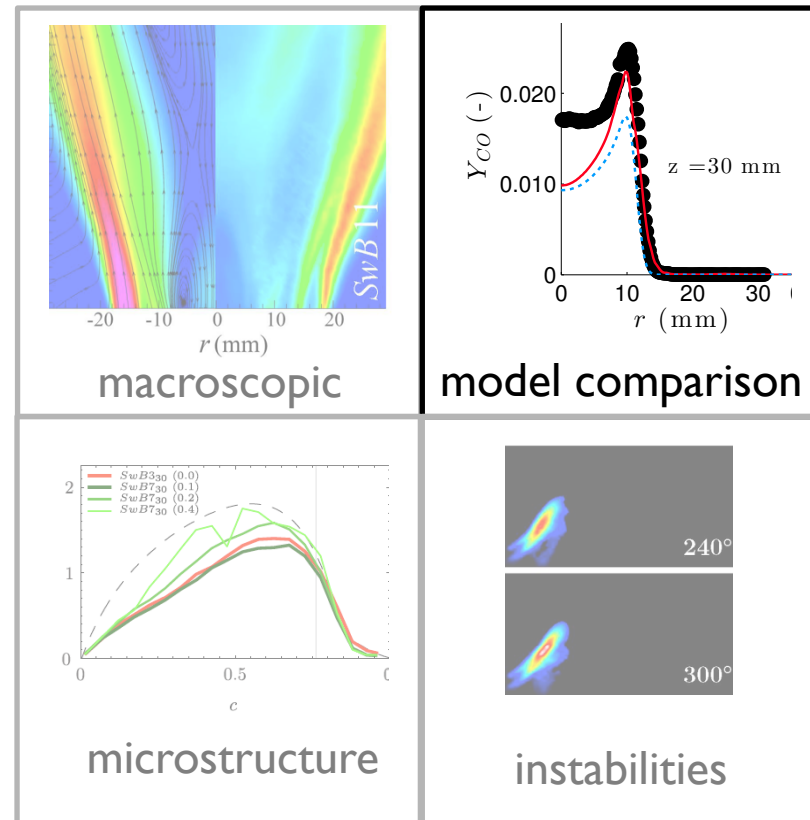
More H than C diffuses towards the reactants
Reactants swept downstream by axial flow

Differential diffusion affects definition of ϕ at peak heat release



Katta & Roquemore, PCI 34 (2013)
doi:10.1016/j.proci.2012.06.033

Outline: Effects of Stratification

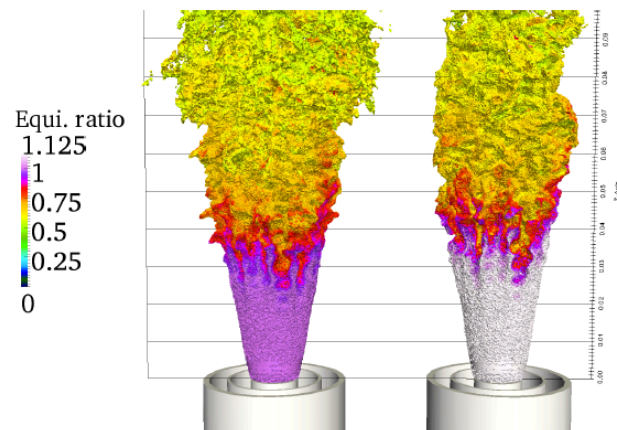


Comparison with LES models

..... CORIA

— ECP

— Duisburg



[1] Nambully, Domingo, Moureau, Vervisch, C&F 2013, under review

FTF-PDF (F-TACLES [2])

Tabulated source for *differential diffusion*

Mercier & Fiorina

[2] Auzillon, P., Gicquel, O., Darabiha, N., Veynante, D. & Fiorina, B. Combustion and Flame 159 (8), 2704 – 2717. (2013)

FTF-PDF (F-TACLES)

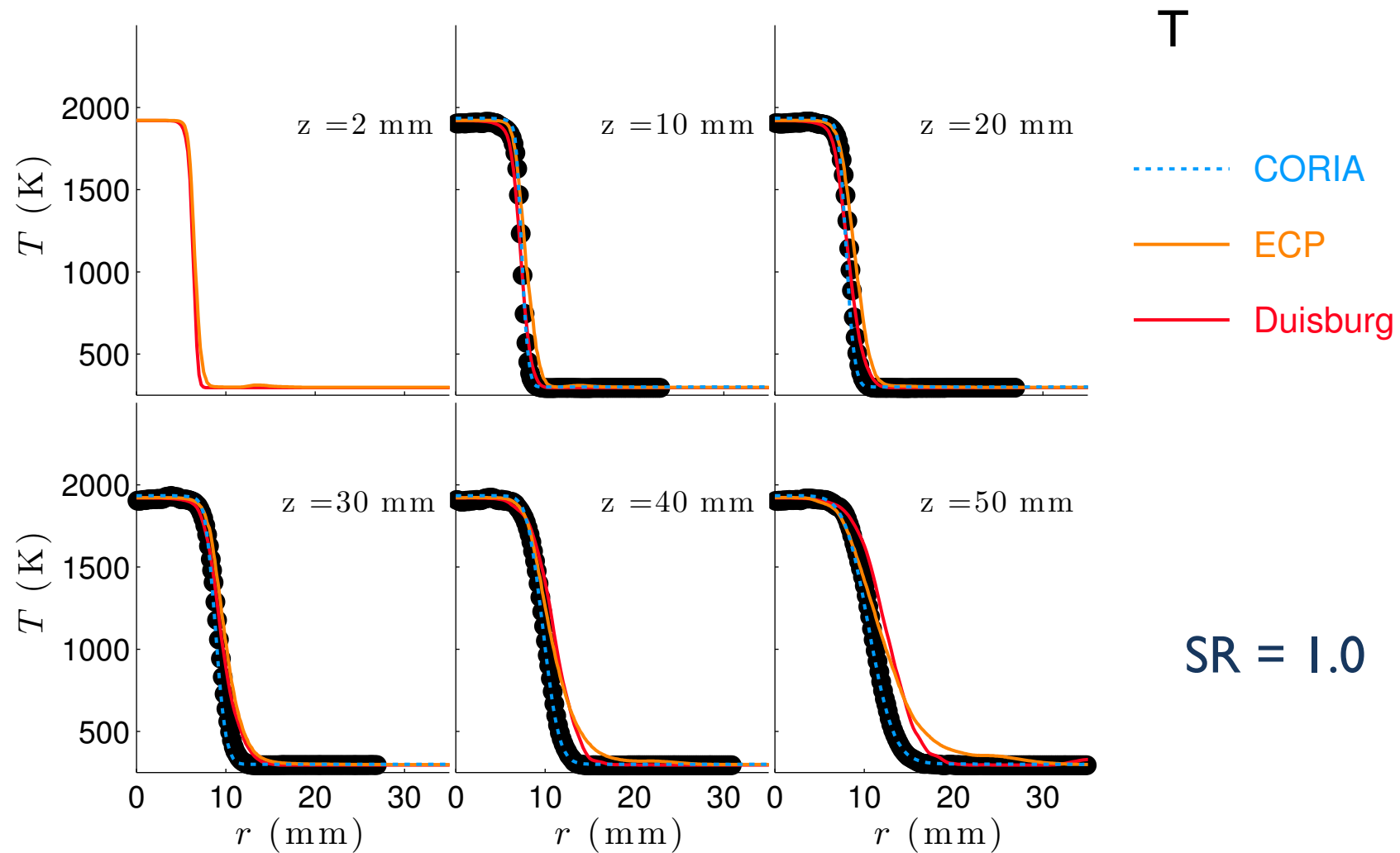
Proch & Kempf

[3] Kuenne, G., Ketelheun, A. & Janicka, J. Combustion and Flame 158 (9), 1750-1767. (2011)

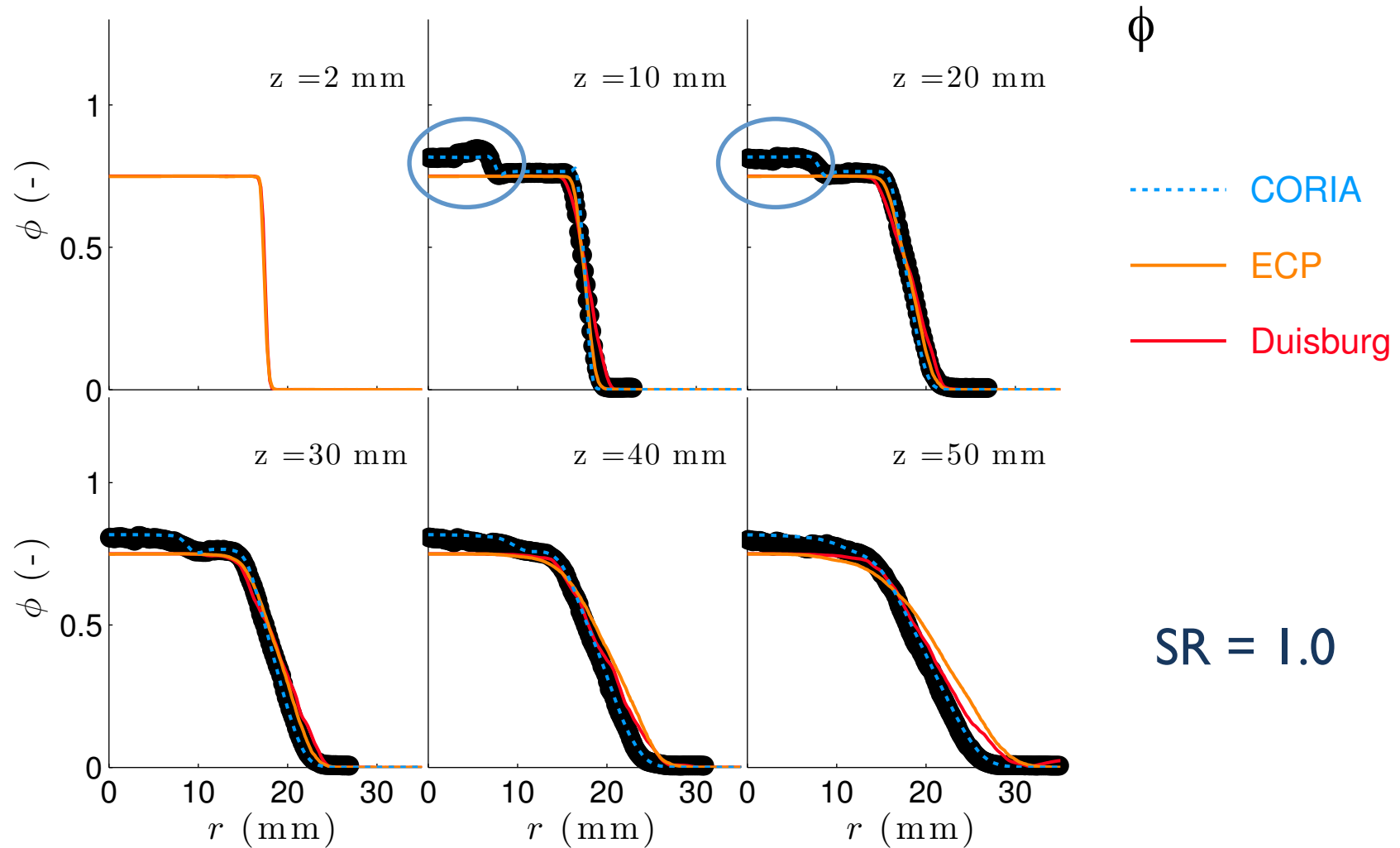
ATF-FGM

Adiabatic bluff body

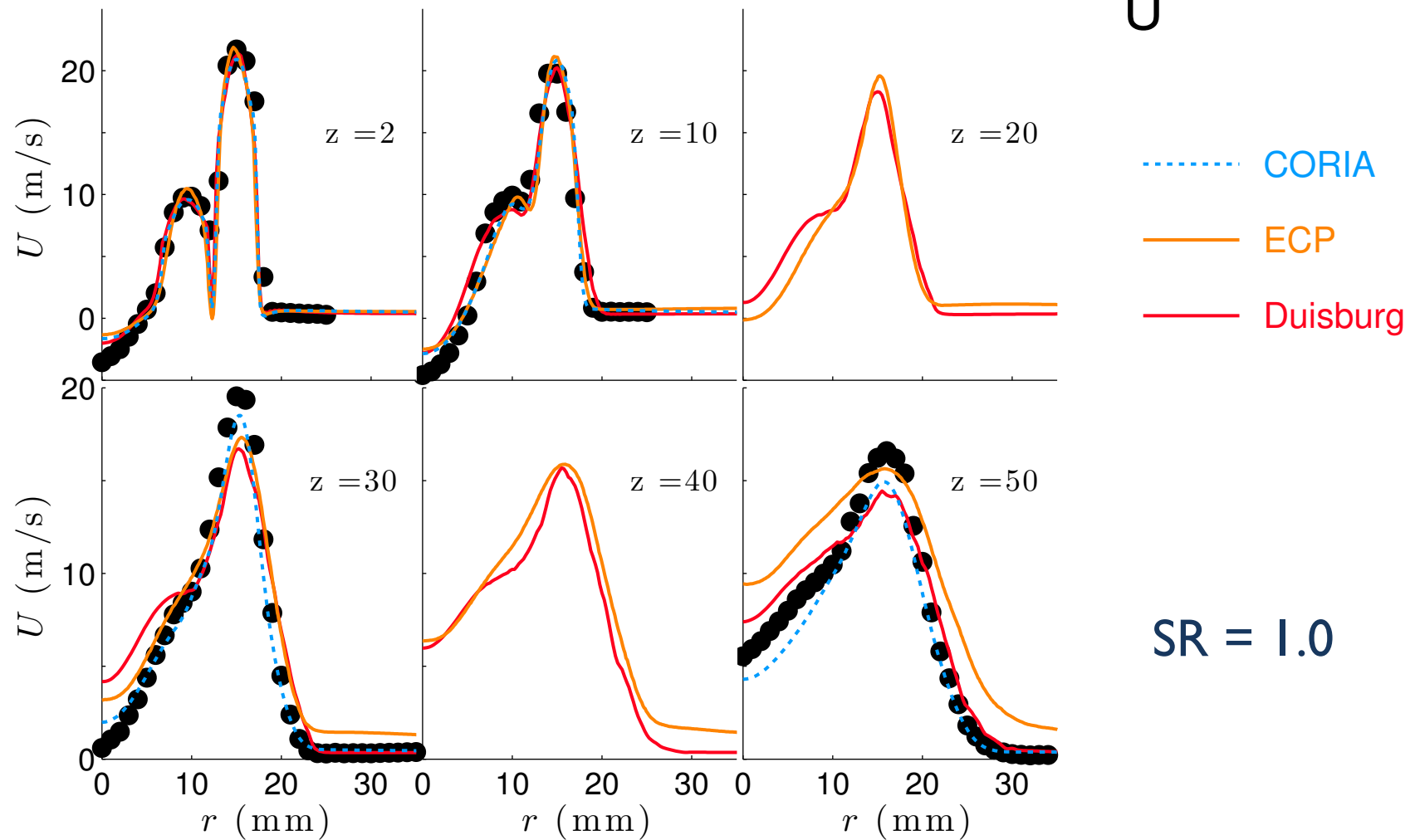
LES Simulations – Premixed, No swirl



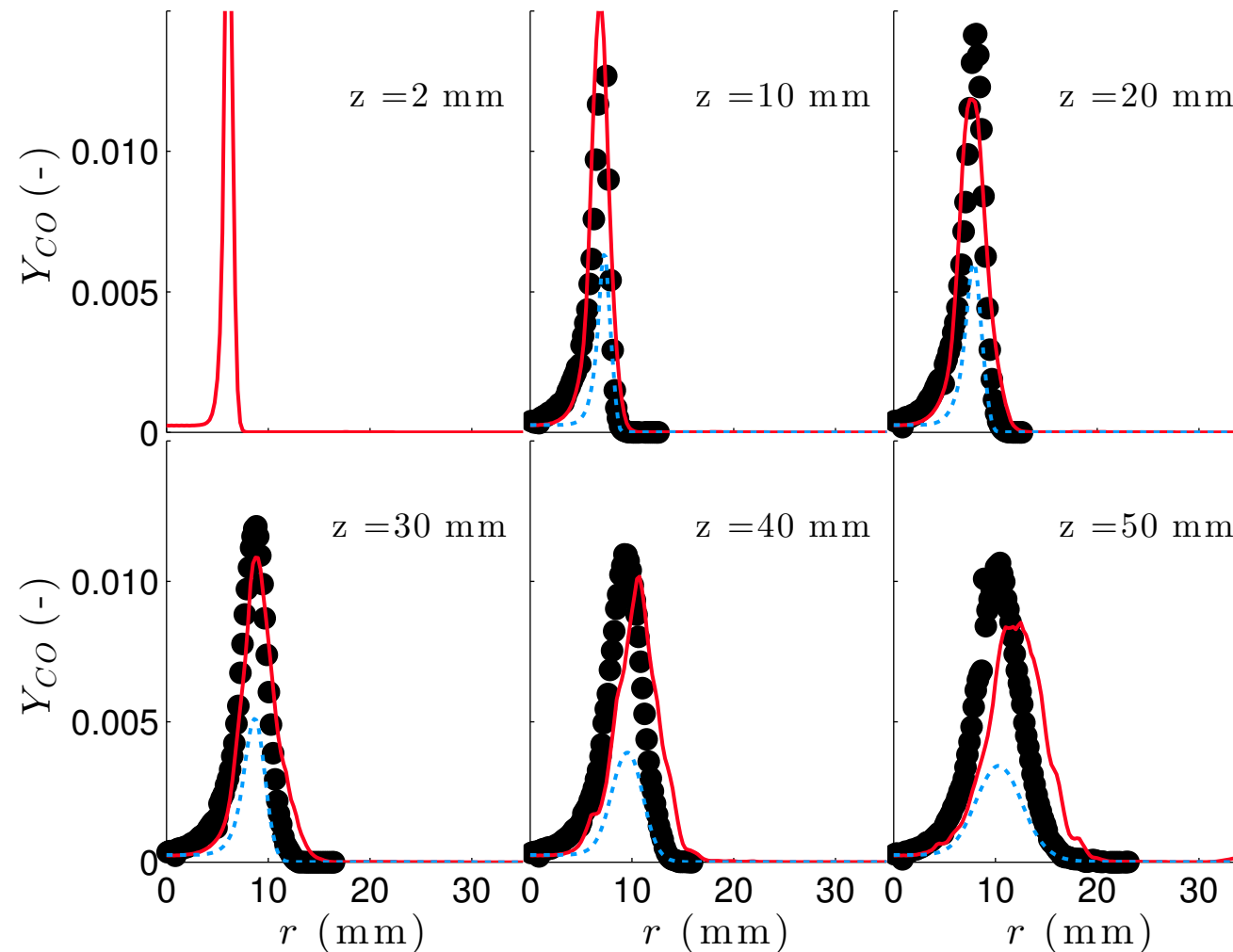
LES Simulations – Premixed, No swirl



LES Simulations – Premixed, No swirl



LES Simulations – Premixed, No swirl

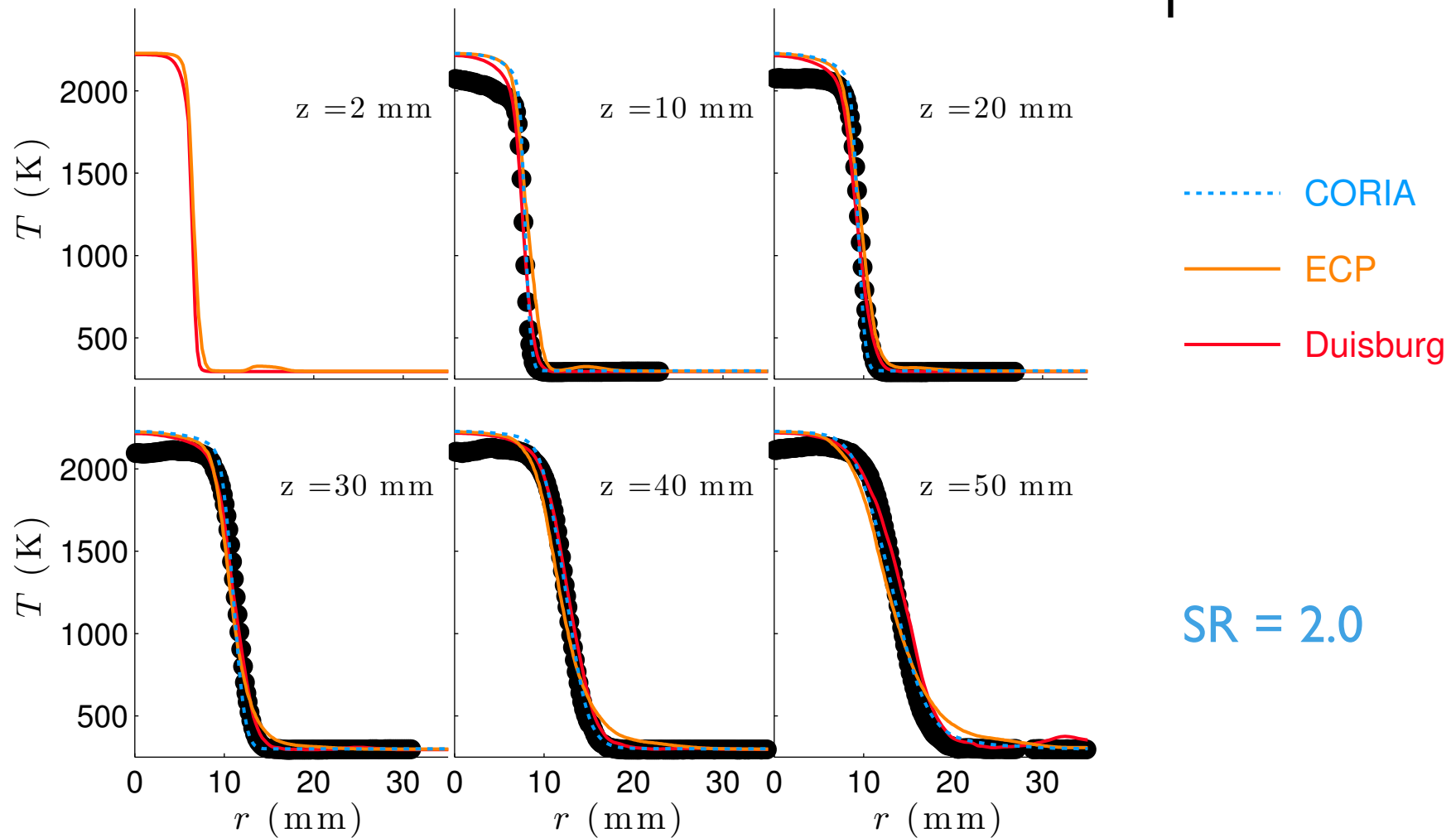


CO

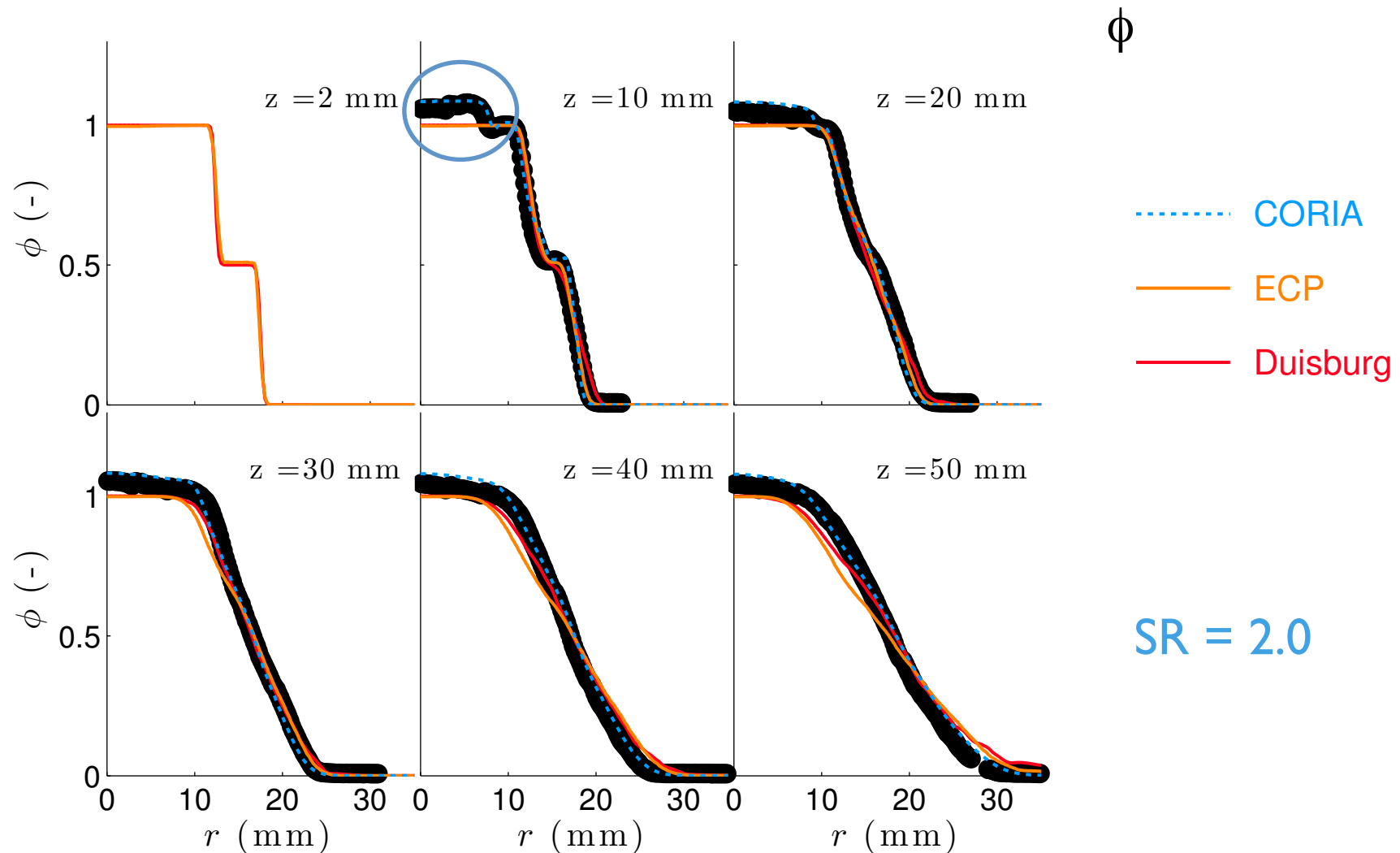
--- CORIA
— ECP
— Duisburg

SR = 1.0

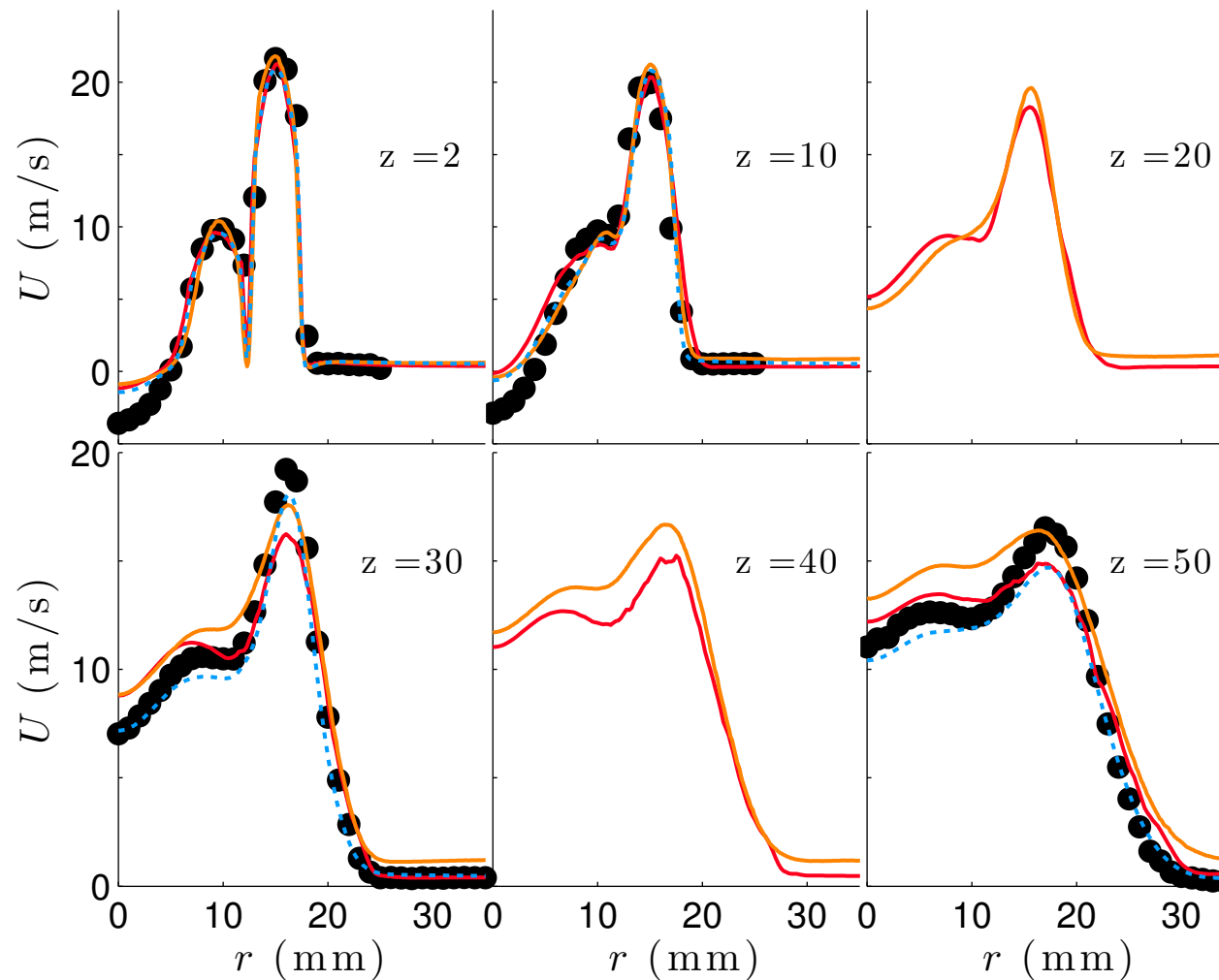
LES Simulations – SR=1.00/0.50, No swirl



LES Simulations – SR=1.00/0.50, No swirl



LES Simulations – SR=1.00/0.50, No swirl

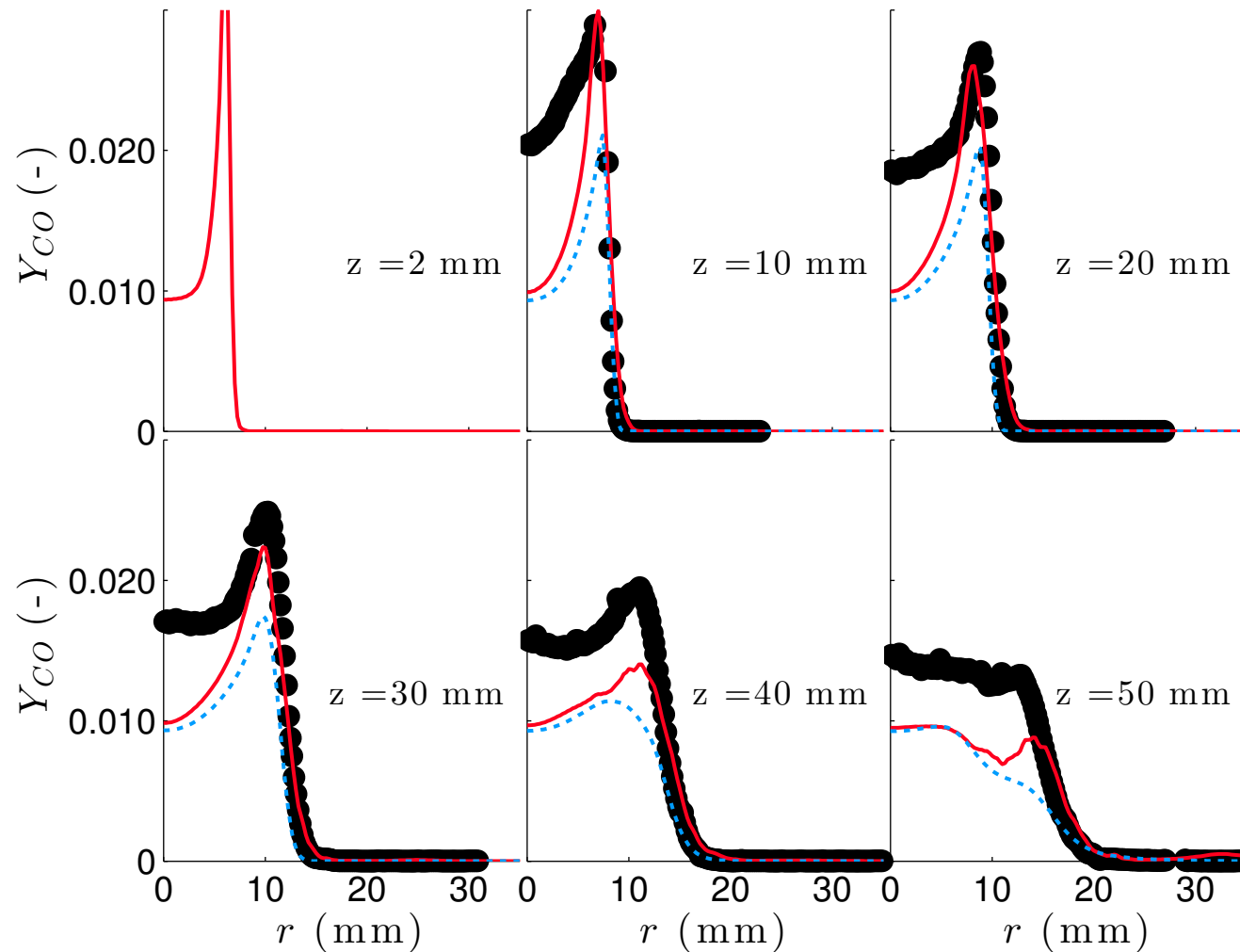


U

..... CORIA
—— ECP
—— Duisburg

SR = 2.0

LES Simulations – SR=1.00/0.50, No swirl



CO

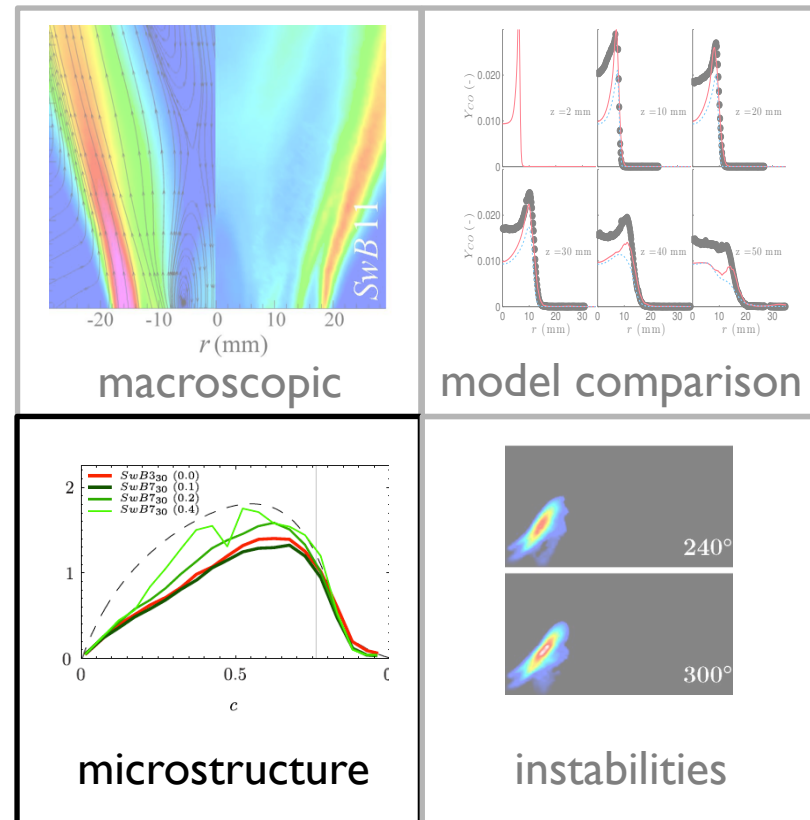
--- CORIA

— ECP

— Duisburg

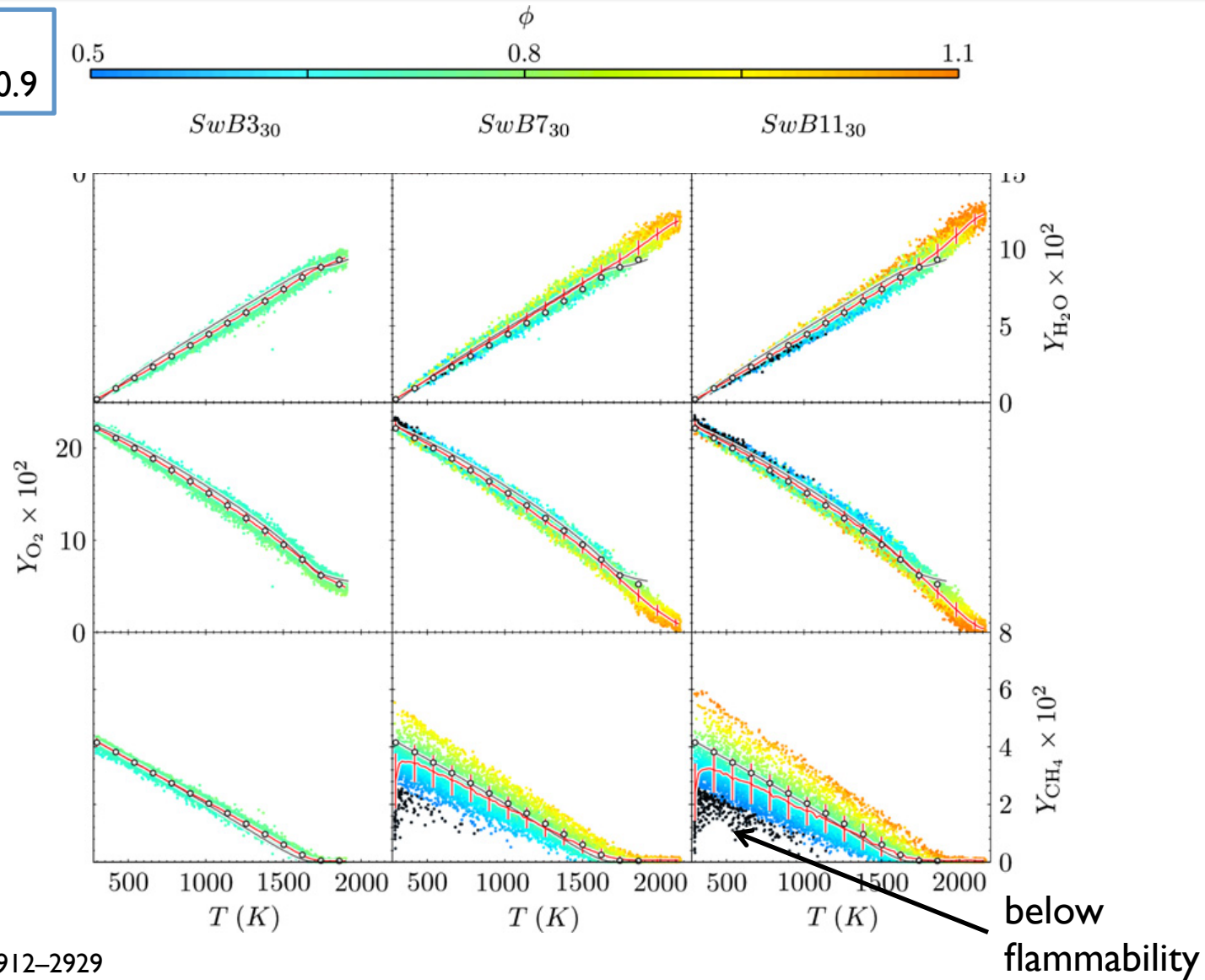
SR = 2.0

Outline: Effects of Stratification

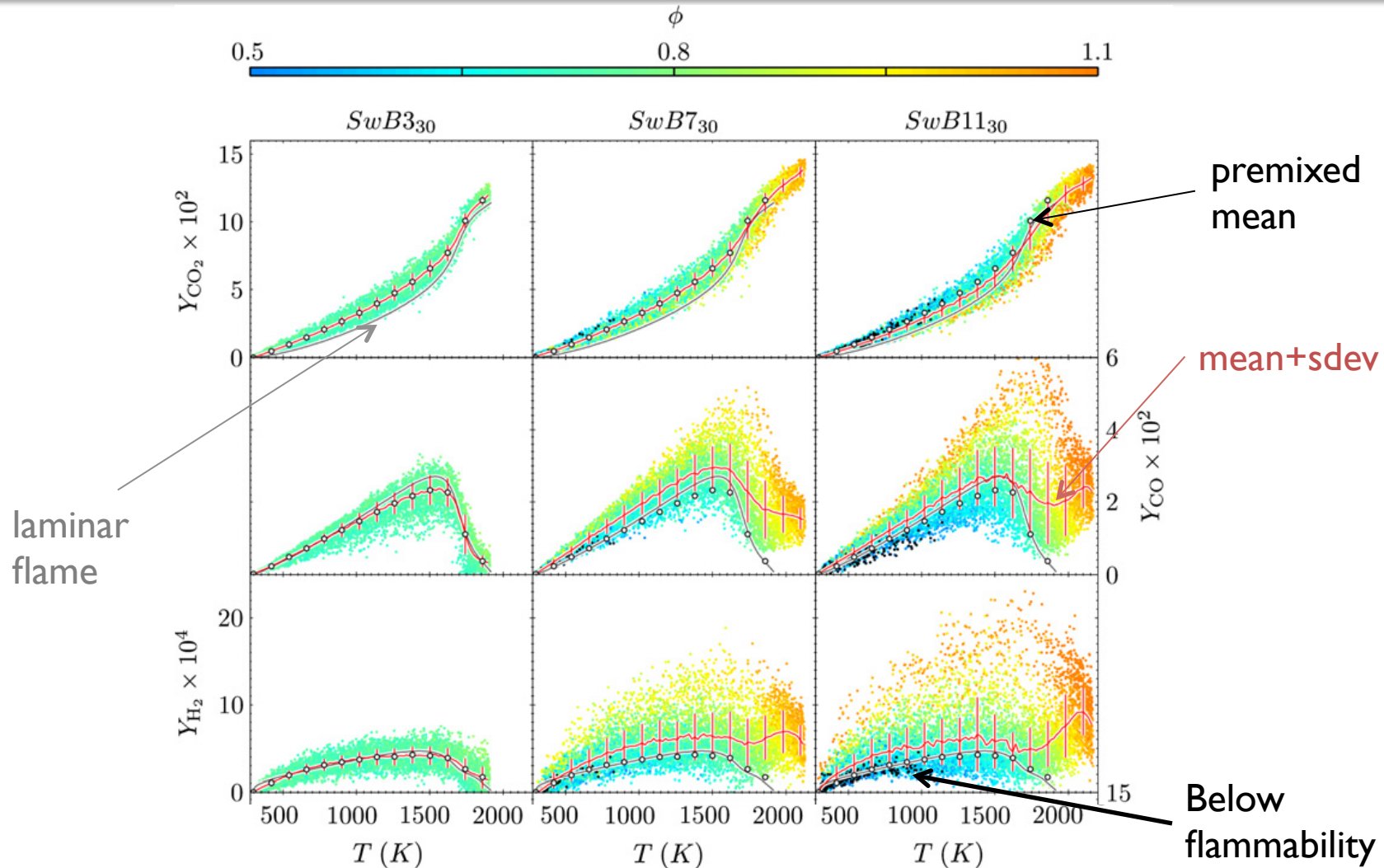


State space for species profiles: swirl cases

-- : mean
+ LF : $0.1 < \Delta\phi/\phi < 0.9$

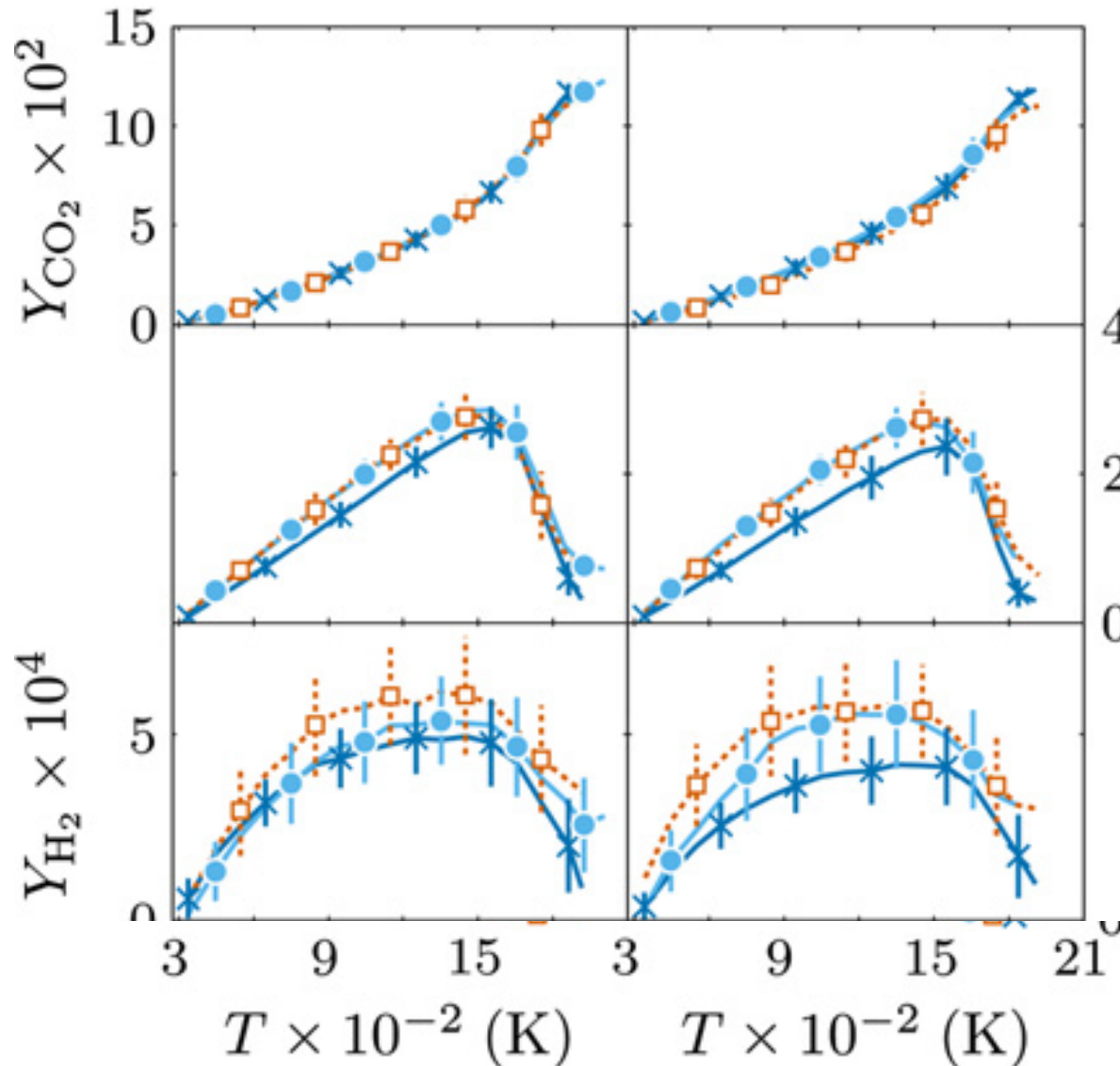


State space in species profiles: swirl cases



Mean flame structure well captured by laminar unstrained flame
Can we separate the effects of equivalence ratio?

Selected conditioned scalar measurements



\times SwB240 \times SwB330
 \circ SwB640 \circ SwB730
 \square SwB1040 \square SwB1130

All swirl cases
 2.5% $\phi = 0.77$ (premixed)

State space similar to premixed

Microscale: local measures of reactivity: Progress of reaction, SDF and χ

$$c = \frac{T - T_0}{T_e(\phi) - T_0}$$

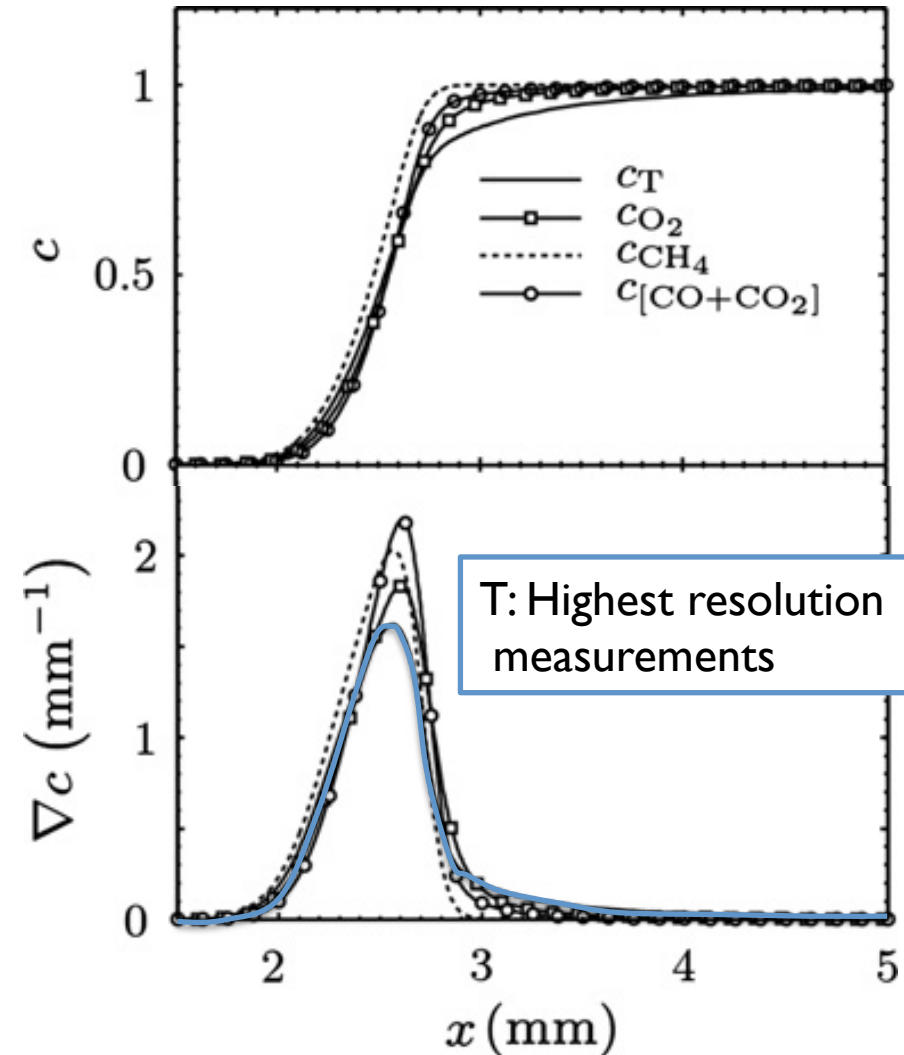
Progress of reaction
(extent of reaction completion)

∇c Surface Density Function
(local flame surface density)

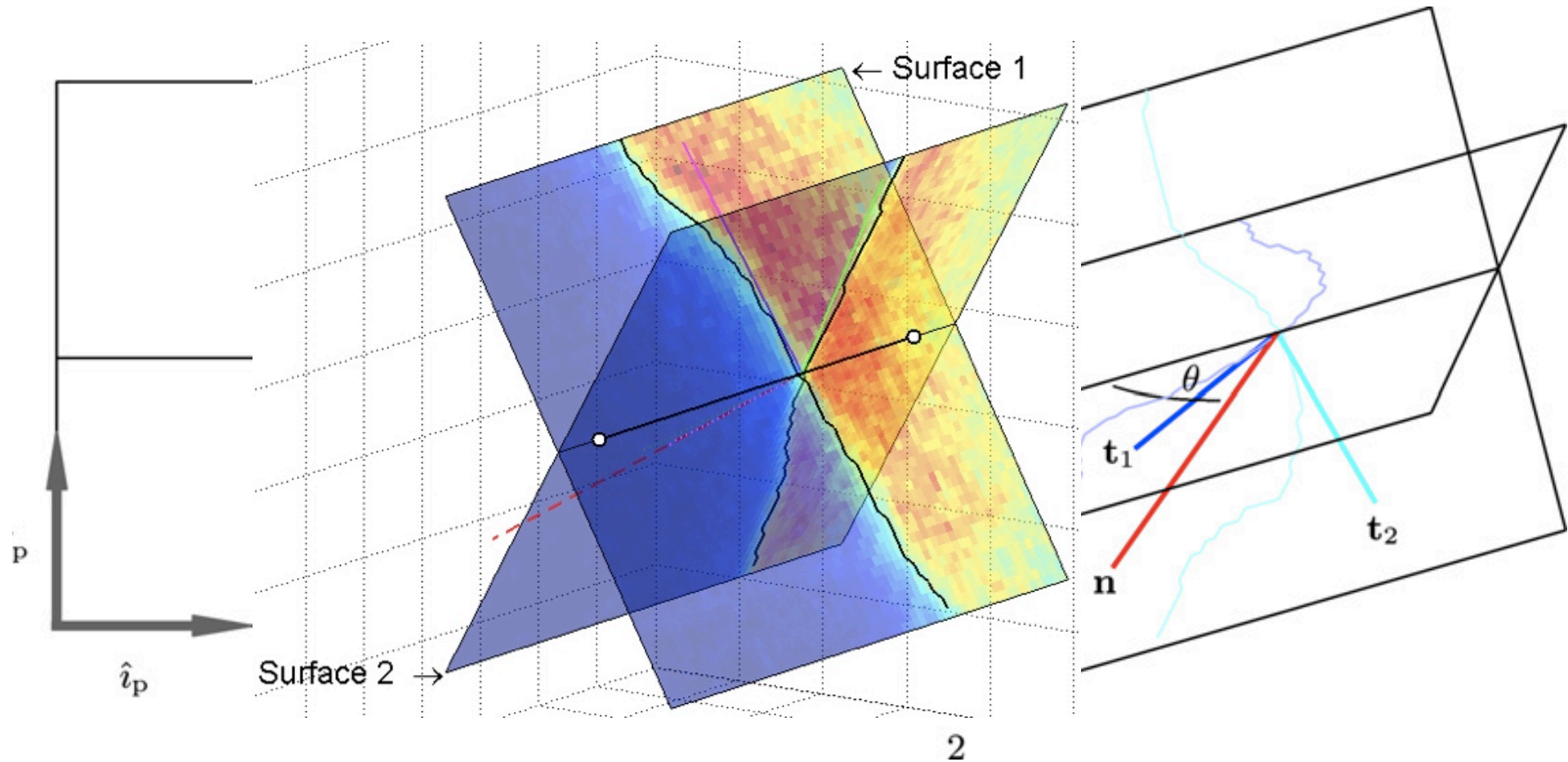
$$\chi = \alpha(T) |\nabla c|^2$$

Scalar dissipation
(scales with reaction rate)

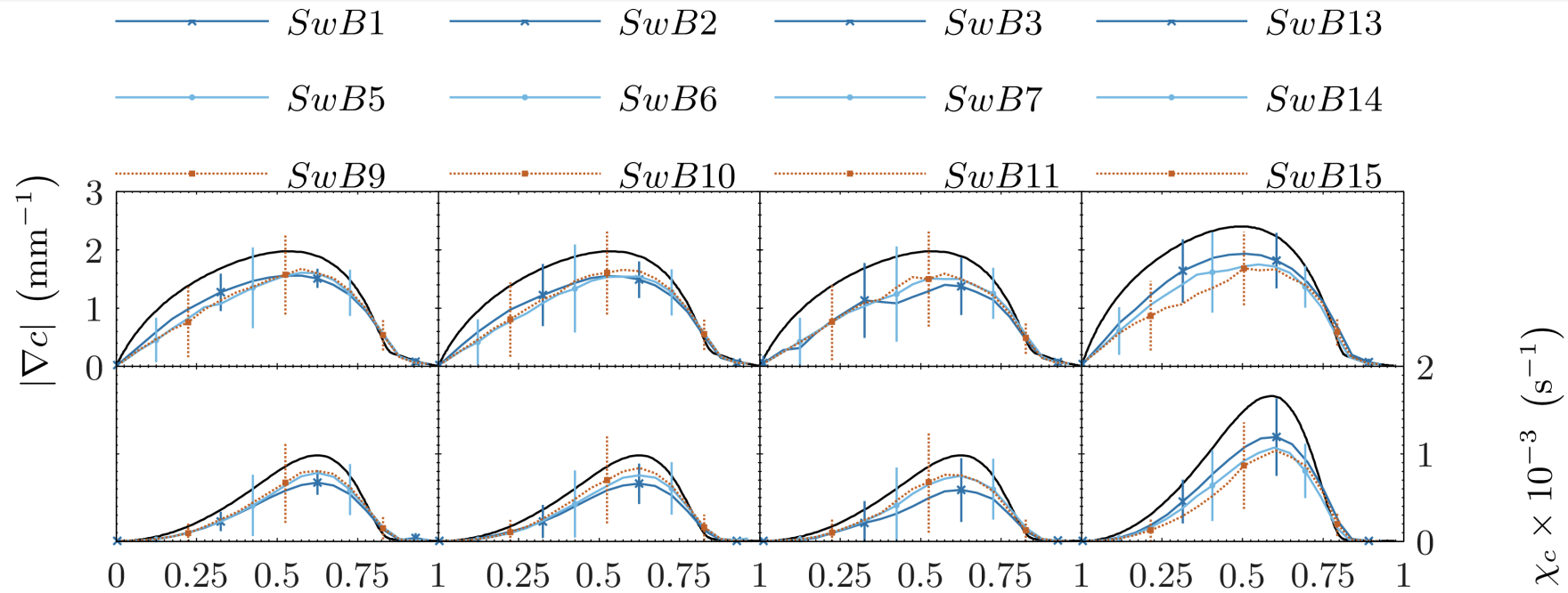
Laminar flame calculations



Gradients: two surface OH



SDF and dissipation for all cases



	c	c	c	c
swirl	0%	25%	33%	0%
	Conditioned at $\phi=0.79$			$\phi = 1.0$
	Bars +/- 2.5% ϕ			

No significant difference between premixed and stratified cases when conditioned for ϕ !

Can we separate by ϕ and its gradient ?

Conditioning ∇c on ϕ and $\nabla\phi$

Select large dataset

Get away from differential diffusion

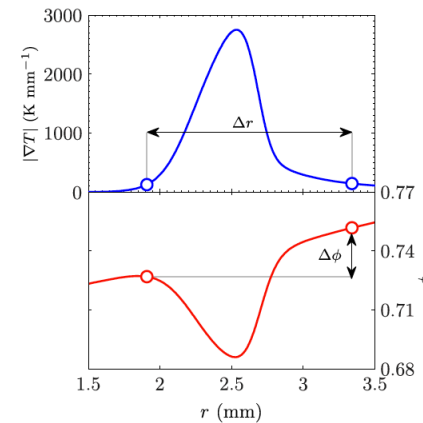
De

- Ch
rel

Get ϕ and $\nabla\phi$:

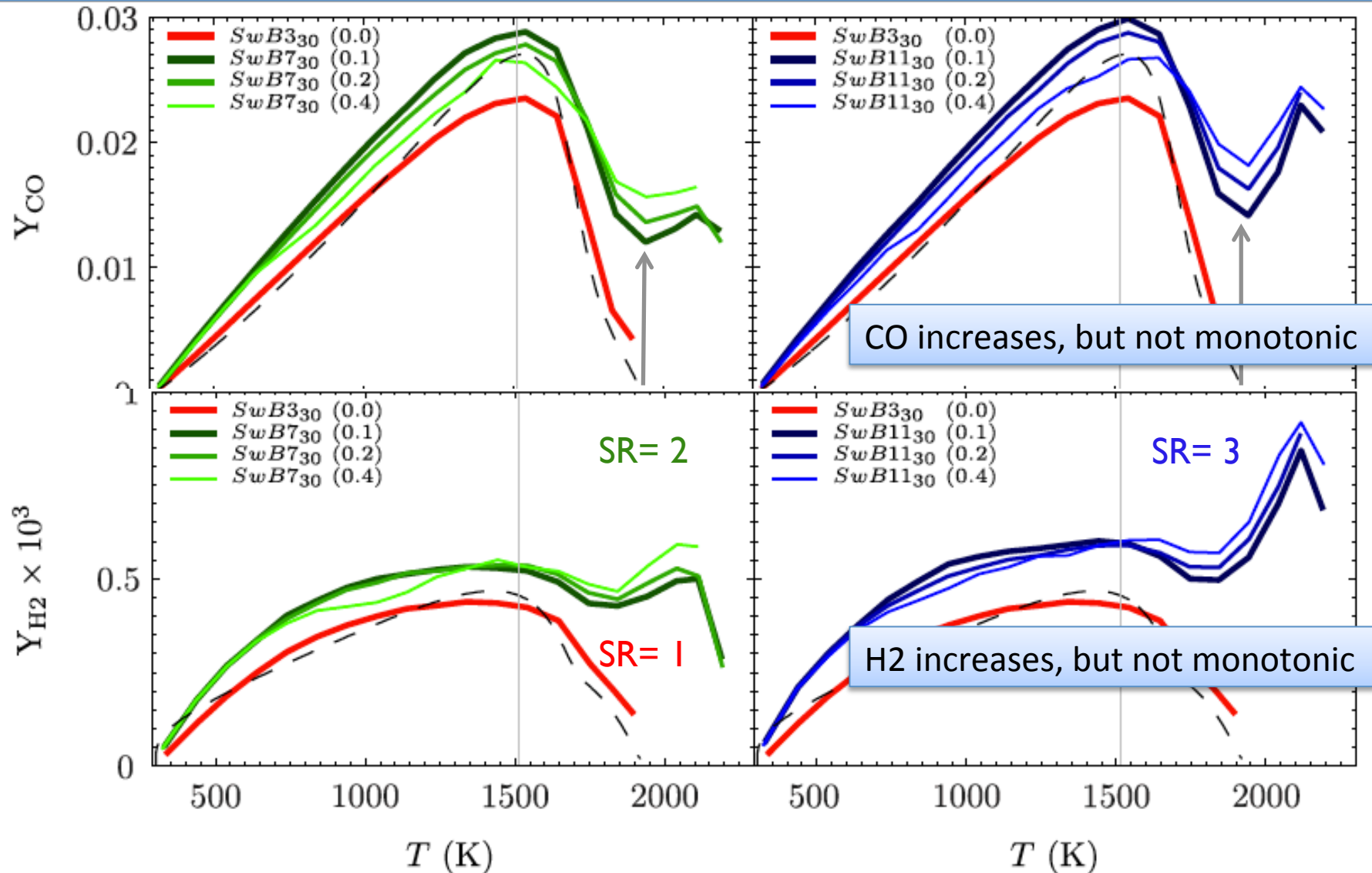
- ϕ interpolate between ± 0.05
of temperature rise

$$\nabla\phi \approx \frac{\Delta\phi}{\Delta r} \frac{1}{\cos\theta}$$

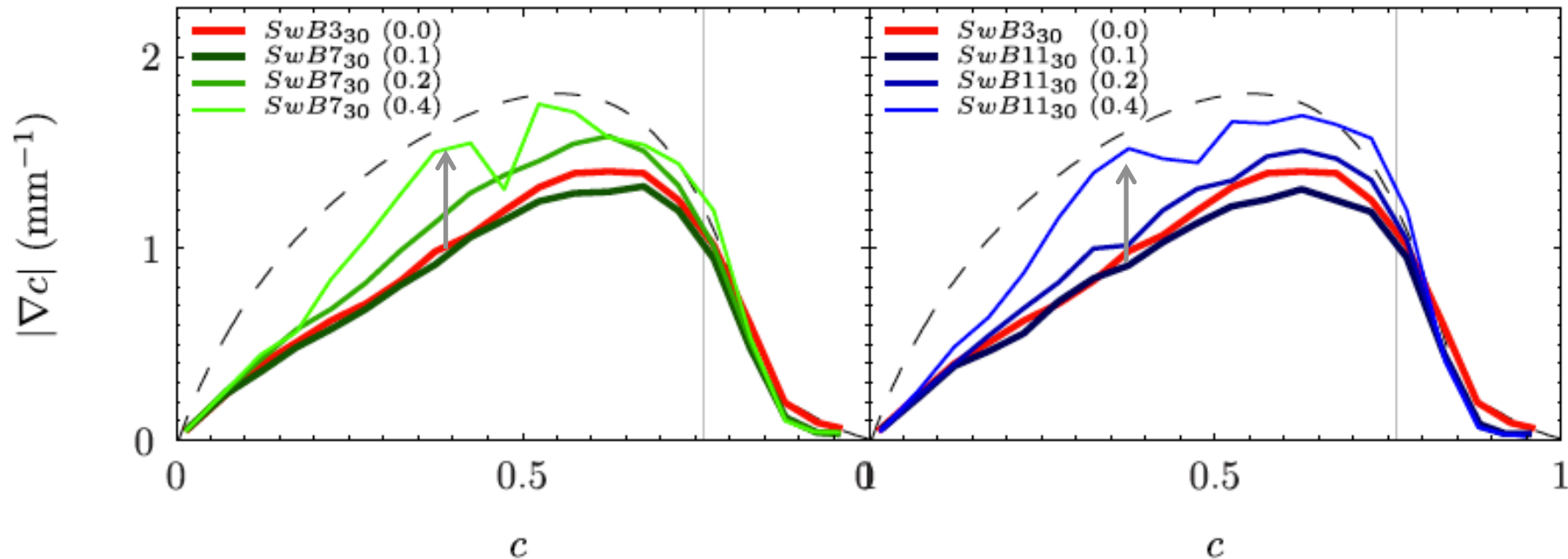


Conditioned scalars: CO and H₂

mean for $\langle \phi; \nabla \phi | \max(Y_{CO}) \rangle$



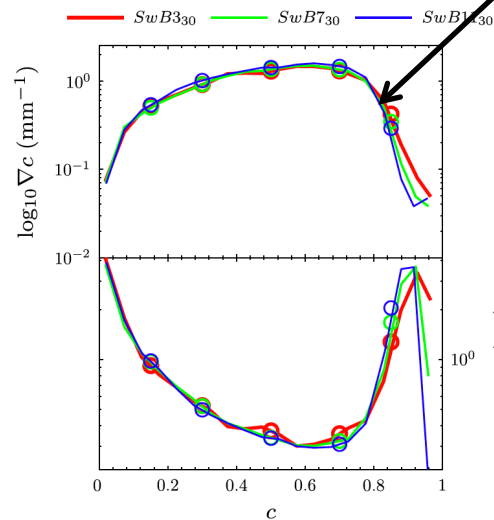
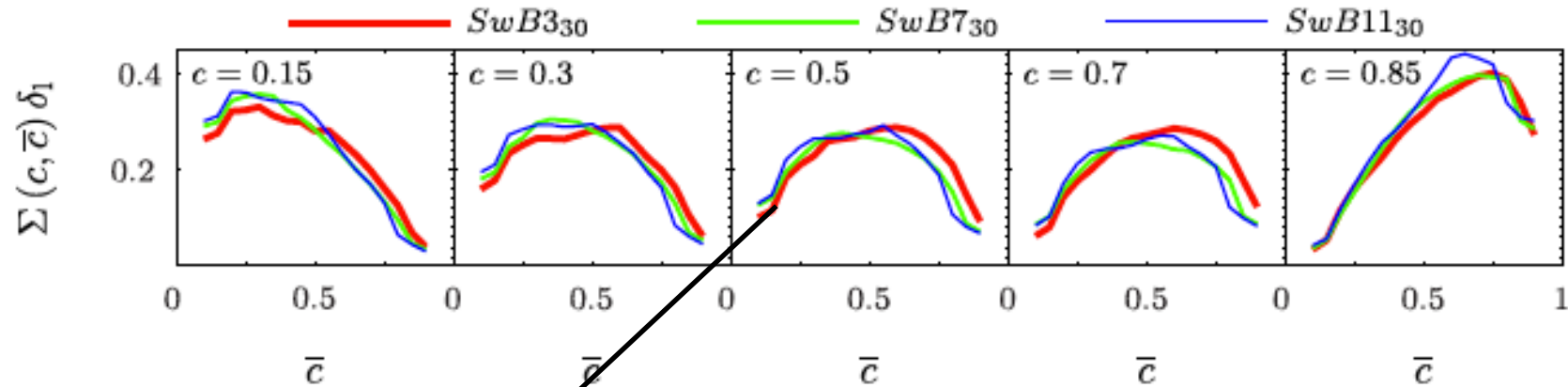
Conditioned values: mean for $\langle \phi; \nabla \phi | \max(Y_{CO}) \rangle$



Finally! This shows that indeed, for a given ϕ at peak heat release, local stratification leads to increased gradients (and, indirectly, higher reaction rate) throughout the flame.

Effect is relatively small, and given the reduced number of events with high stratification, explains why it does not affect averages significantly

Conditioned flame surface density



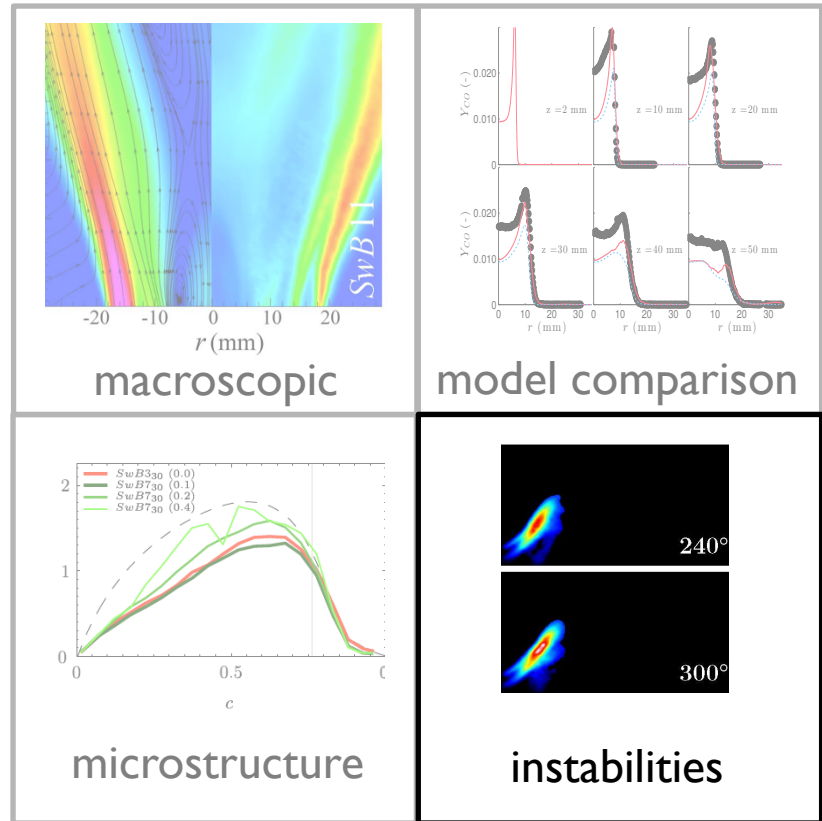
Flame surface density unchanged:

$$\Sigma(c, \bar{c}) = P(c, \bar{c}) \langle |\nabla c| | c \rangle | \bar{c}$$

decreases

increases

Outline: Effects of Stratification

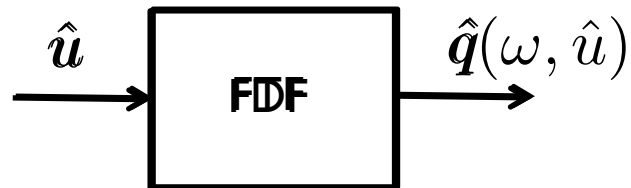
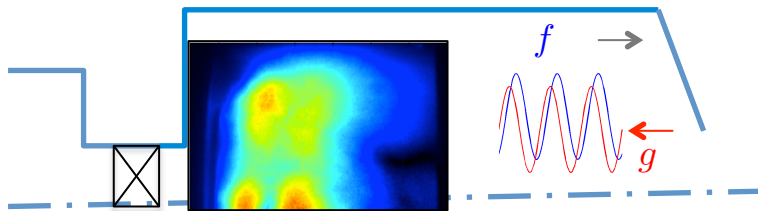


Combustion instabilities

$$\frac{1}{p} \frac{\partial^2 p'}{\partial t^2} - \nabla \cdot \left(\frac{c^2}{p} \nabla p' \right) = (\gamma - 1) \frac{q}{p} \boxed{\frac{D q'}{Dt}}$$

wave propagation

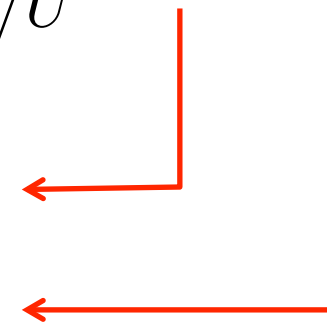
heat release rate per volume



$$F(\omega; \hat{u}/U) \equiv \frac{\hat{q}/q}{\hat{u}/U} \equiv G e^{-i\phi}$$

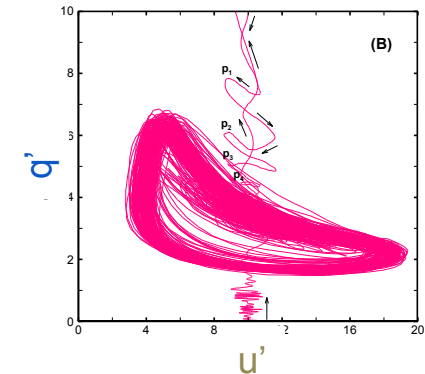
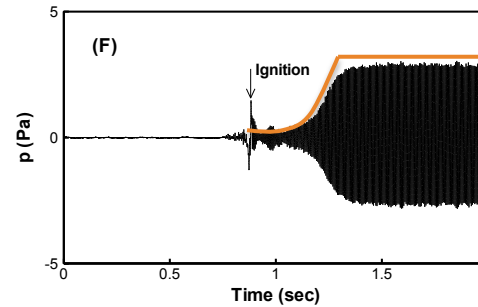
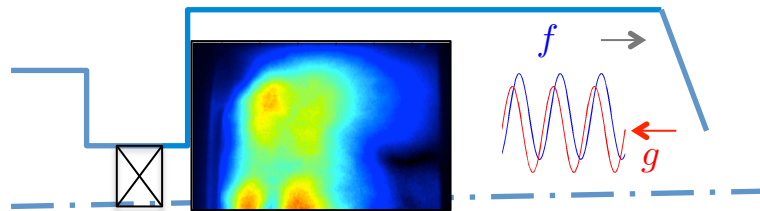
$$G(\omega, \hat{u})$$

$$\phi(\omega, \hat{u})$$

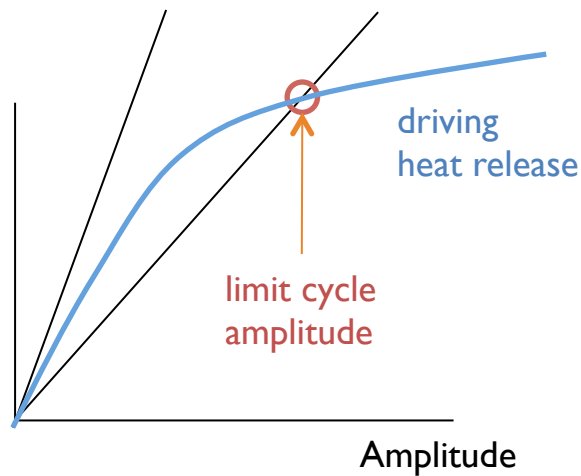


N. Chiriac, J. Fluid Mech., Lett. Soc., 17, 1, 1951
 A.P. Dowling, J. Fluid Mech., 346, 27, 1270, 4, 1997.

Limit cycle – the simple view



energy loss



Kim & Hochgreb, Comb. Flame 159 (2012)

- Self-excited periodic oscillations:
- Net result of matching possible system modes to existing excitation
 - **Limit-cycle = matching point (A,f)**

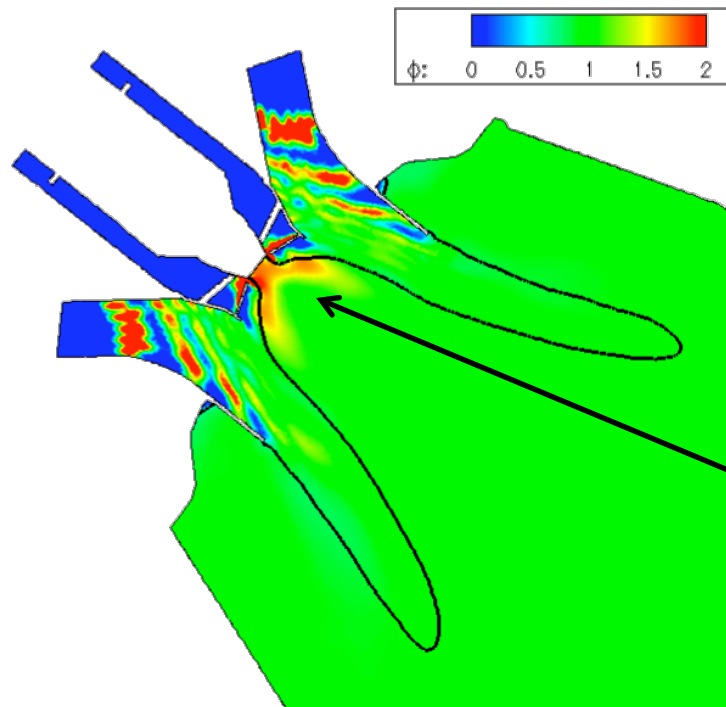
Noiray et al. J. Fluid Mech, 615 (2008)

Dowling. J. Fluid Mech. 346 (1997)

Mean reacting flow fields – CERFACS simulator

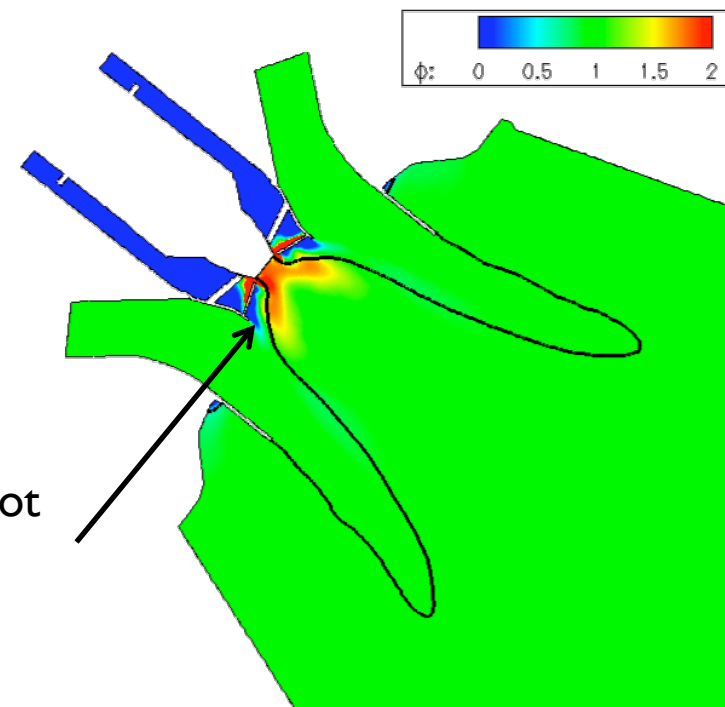
TECH

- Mixture heterogeneities in diagonal swirler
- Quasi-uniform mixture reaches the flame front

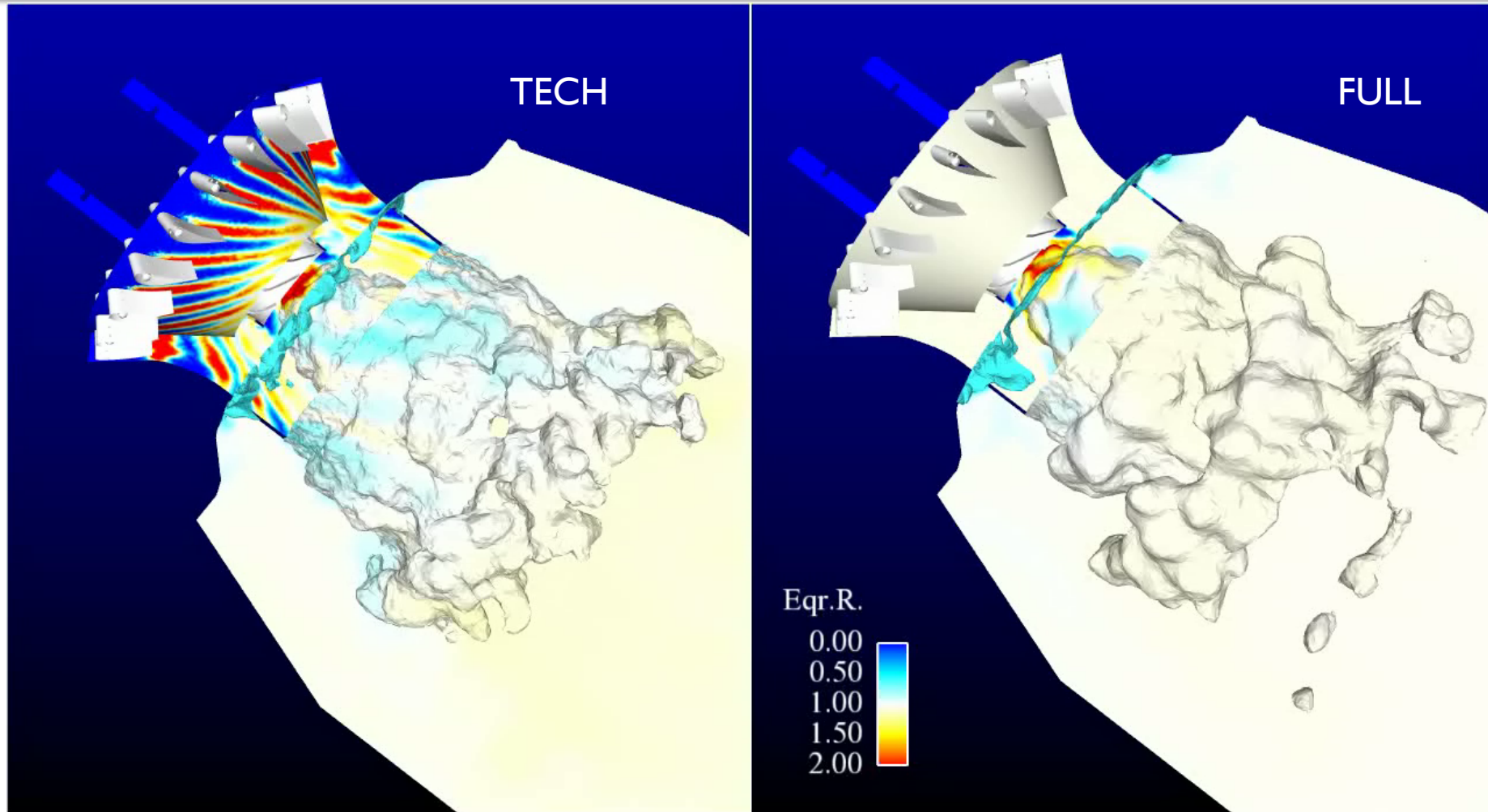


FULL

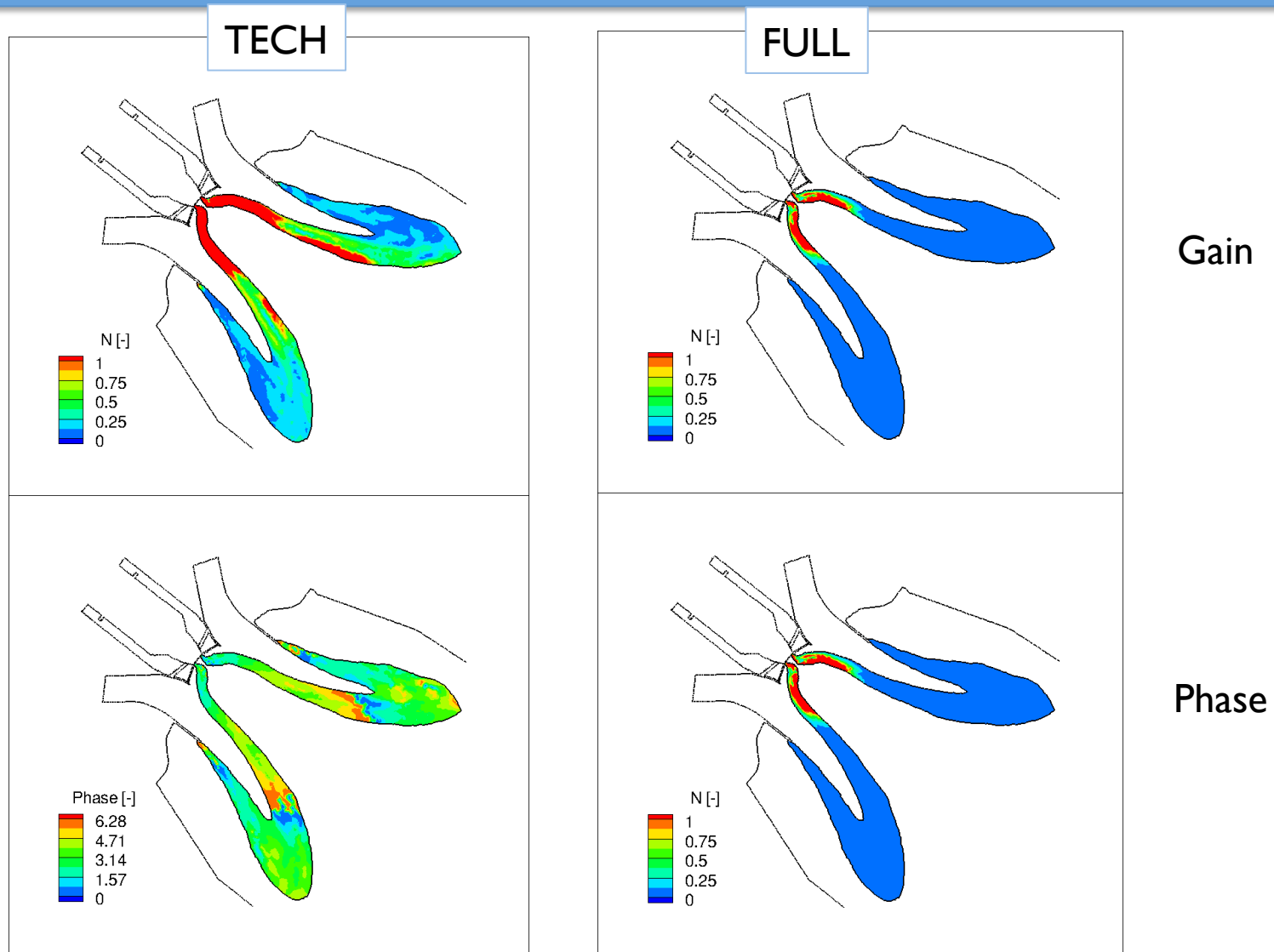
- Uniform mixture in diagonal swirler
- Similar flame



Equivalence ratio fluctuations

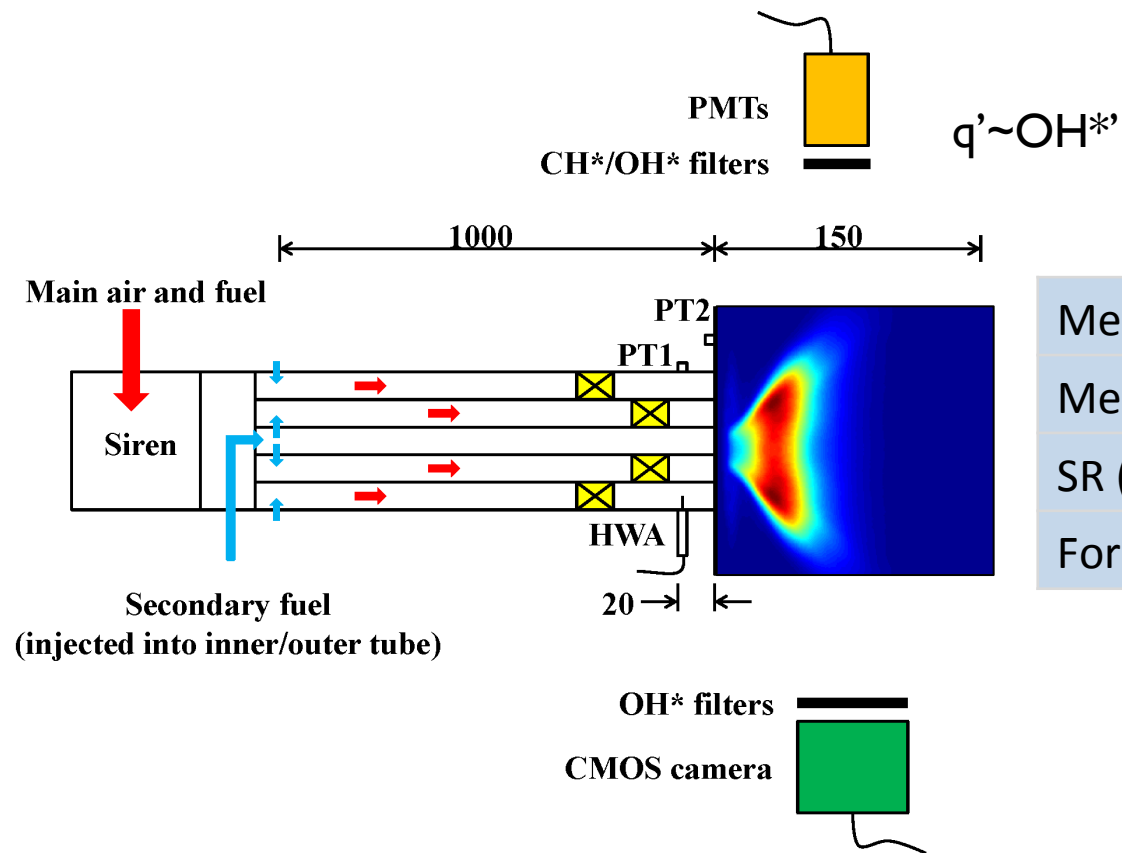


Local Flame Transfer Function



Model Stratified Swirl Burner

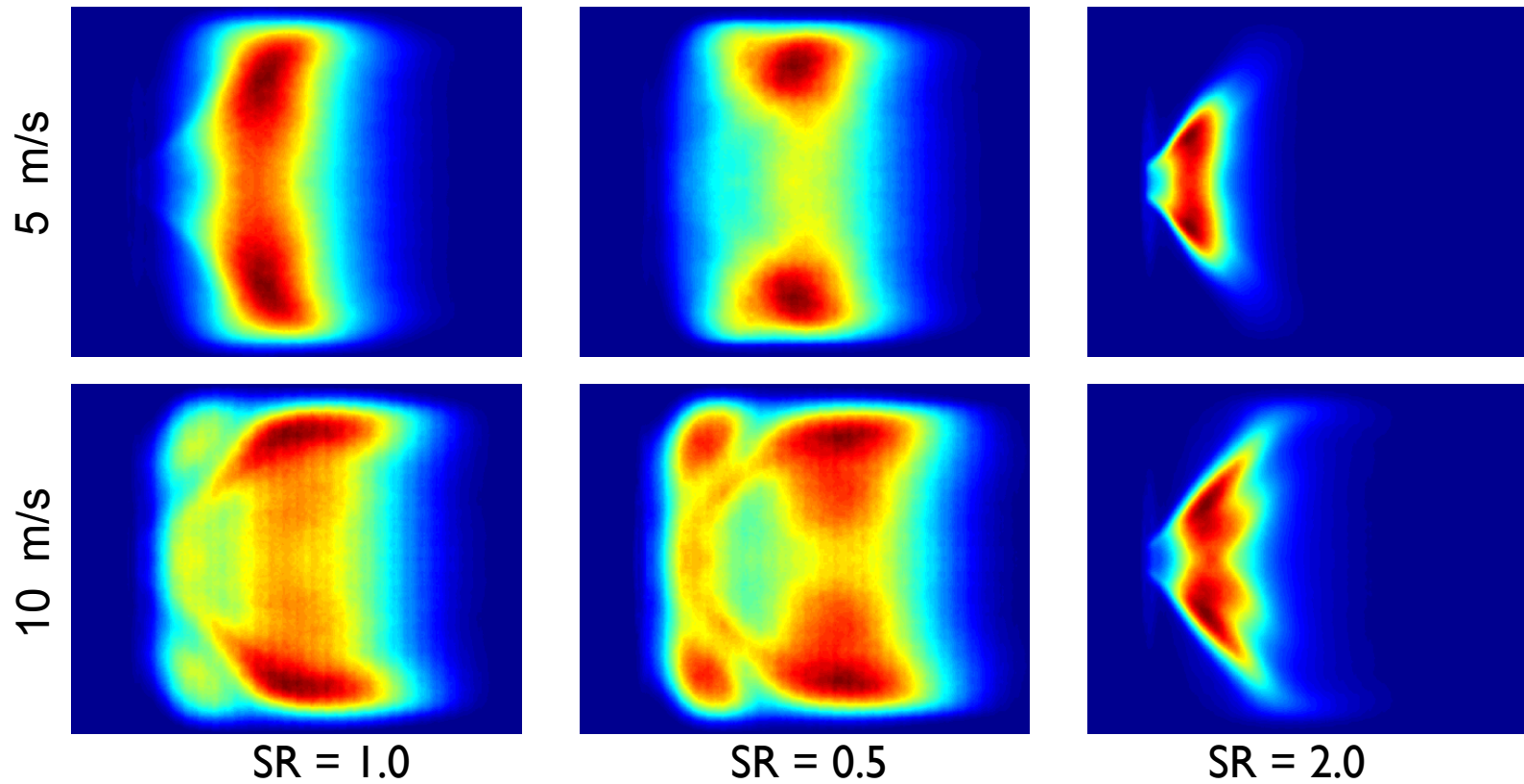
Co-annular swirl passages



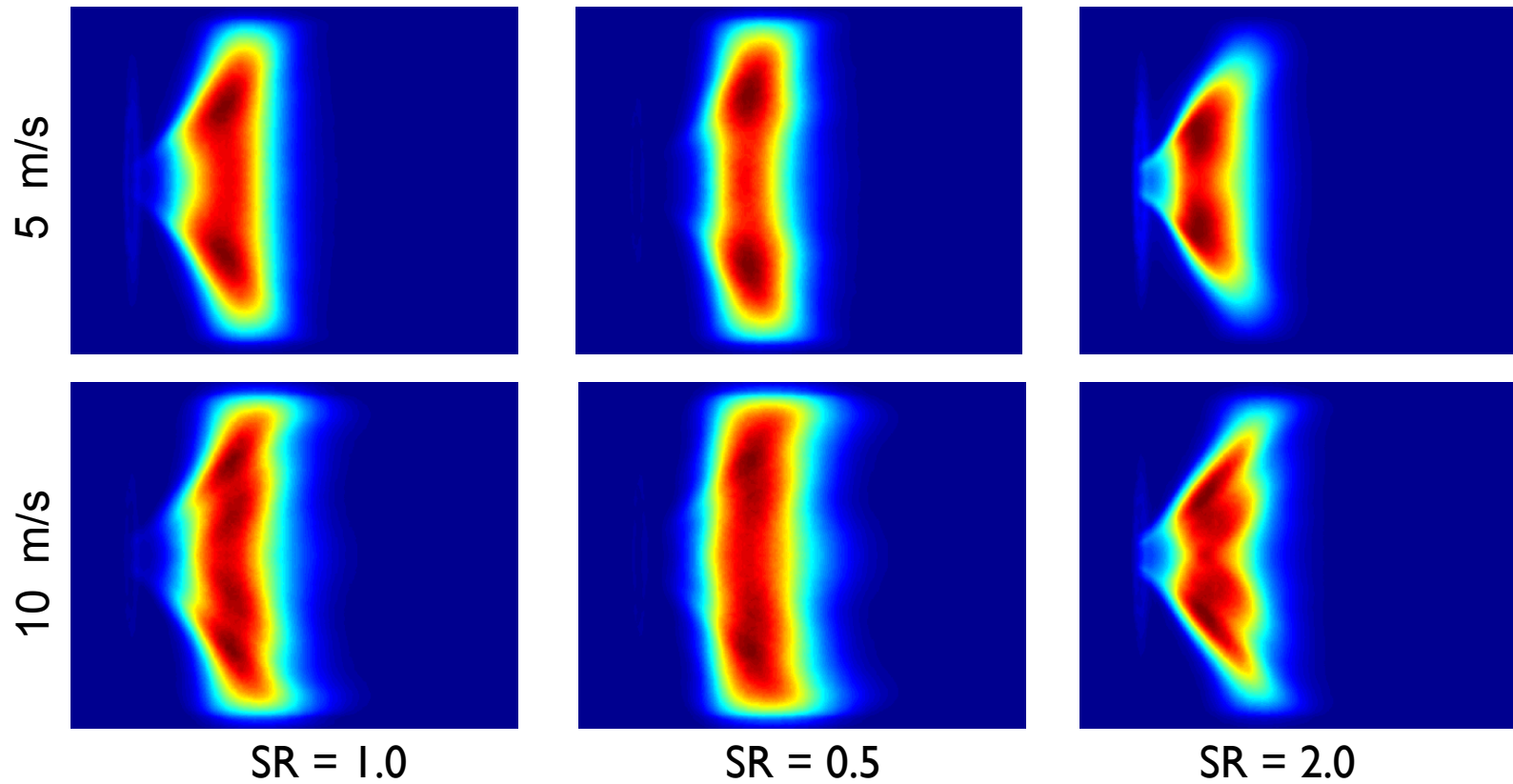
Mean ϕ (-)	0.60, 0.70, 0.80
Mean U (m/s)	5,10
SR (-)	1.0,2.0,3.0
Forcing f (Hz)	60-400

Kim & Hochgreb, C&F 2011a,b, CST 2011
Han & Hochgreb, ECM 2013

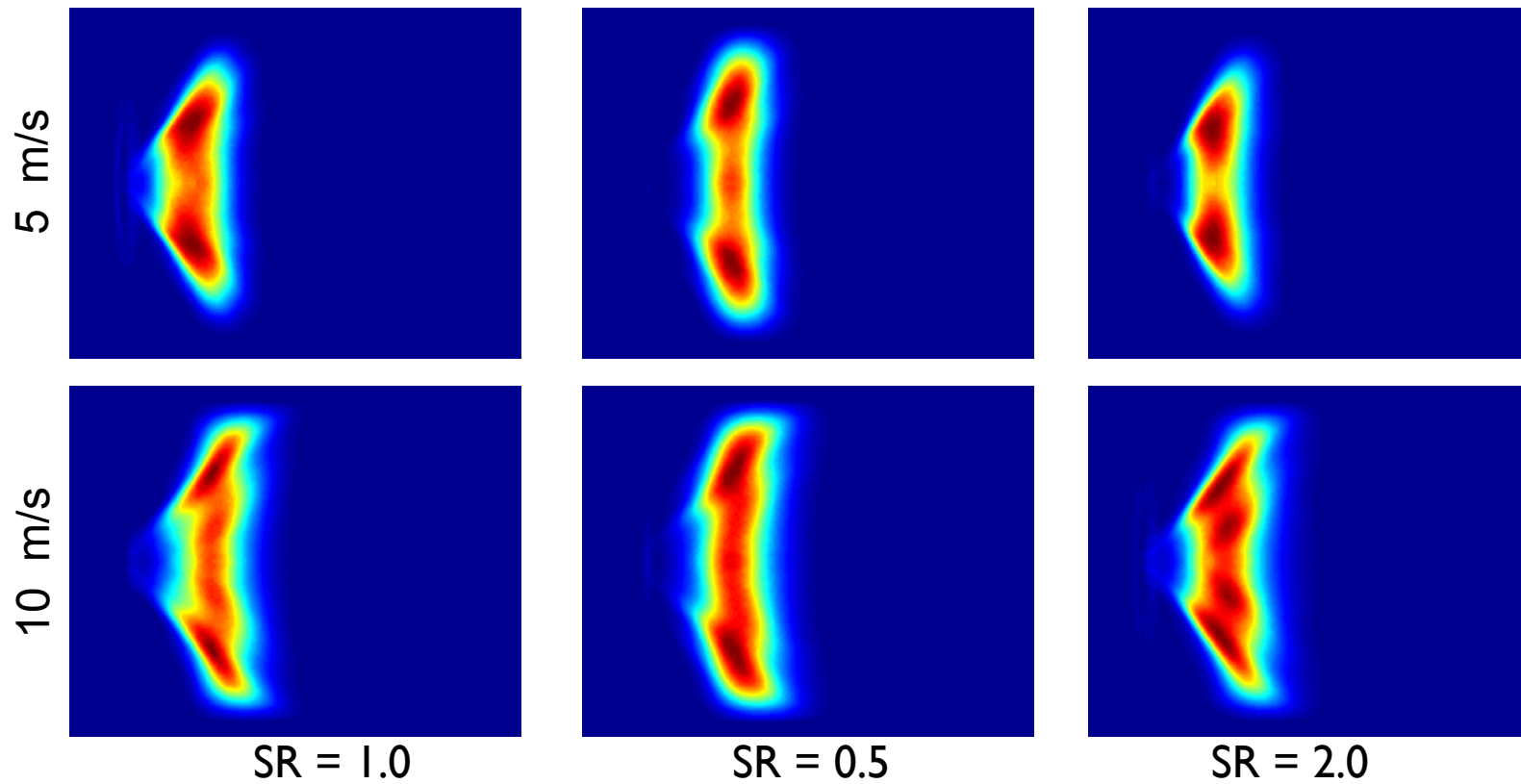
Mean Flame $\text{OH}^* - \Phi_g = 0.60$



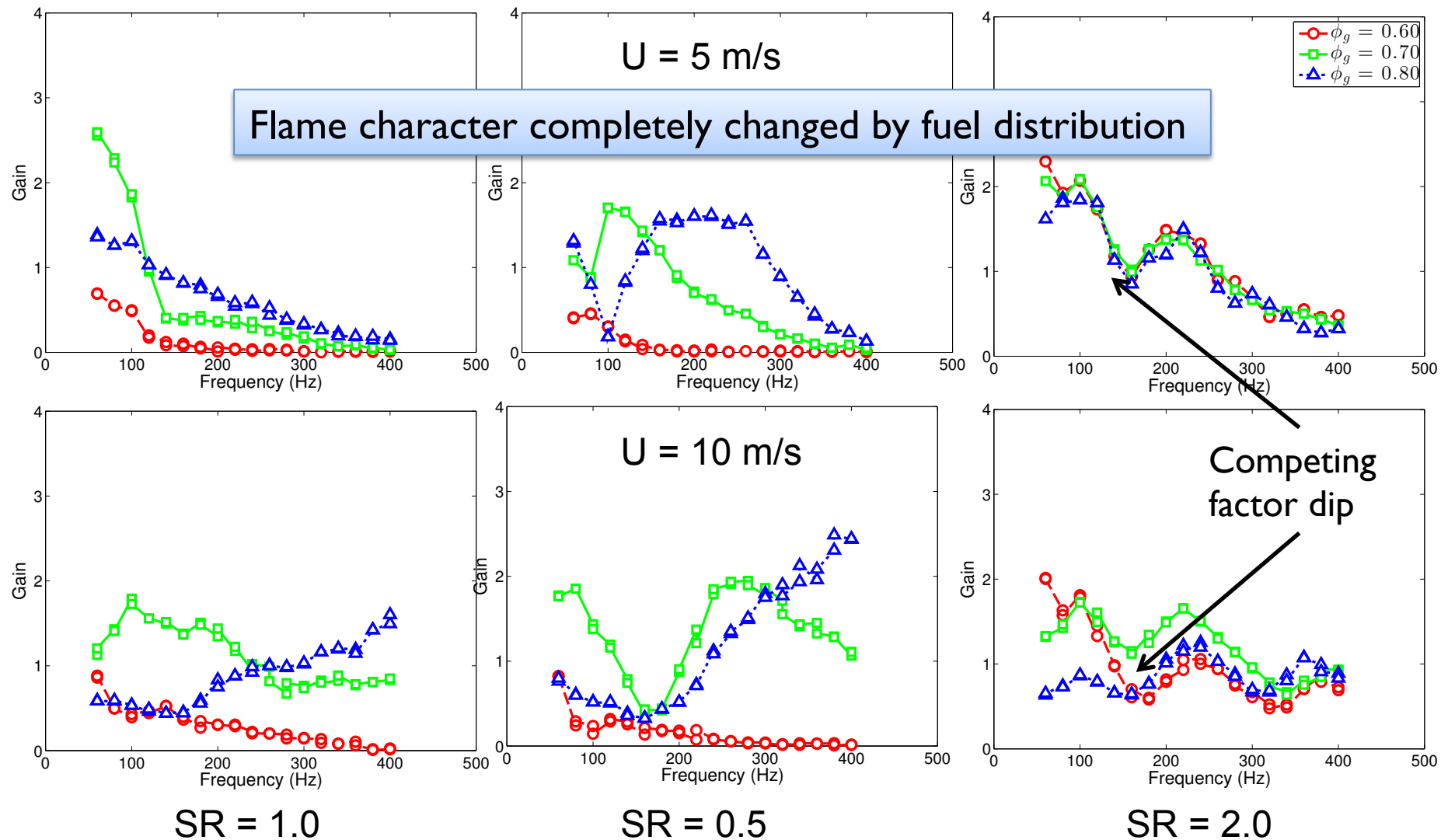
Mean Flame $\text{OH}^* - \Phi_g = 0.70$



Mean Flame $\text{OH}^* - \Phi_g = 0.80$



Flame Transfer Function Gain

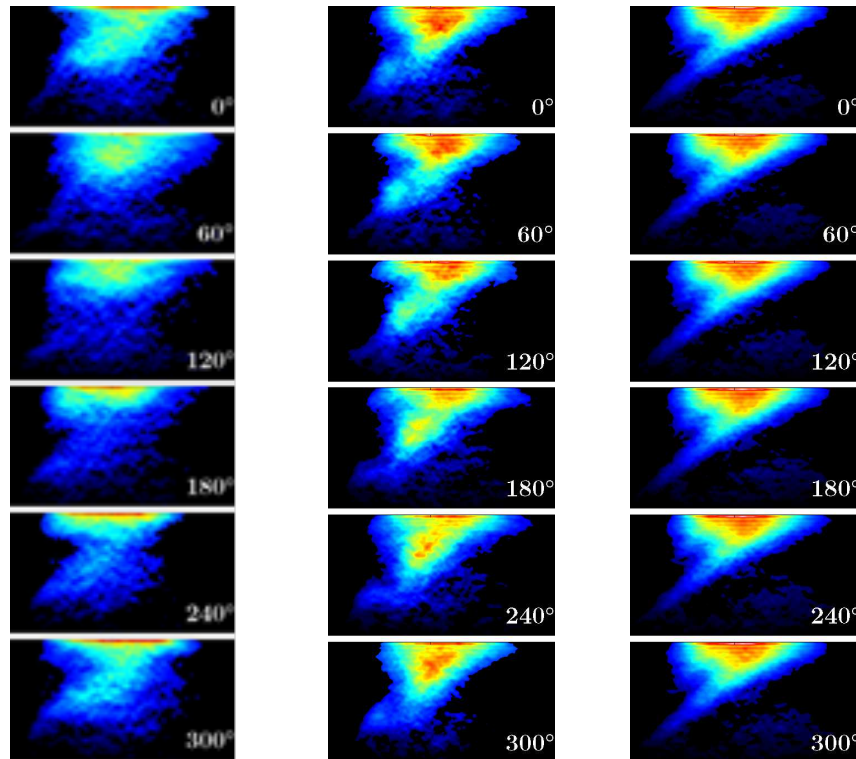


Flame character completely changed by fuel distribution

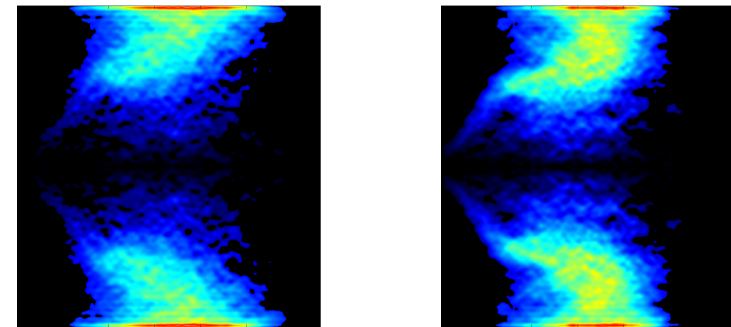
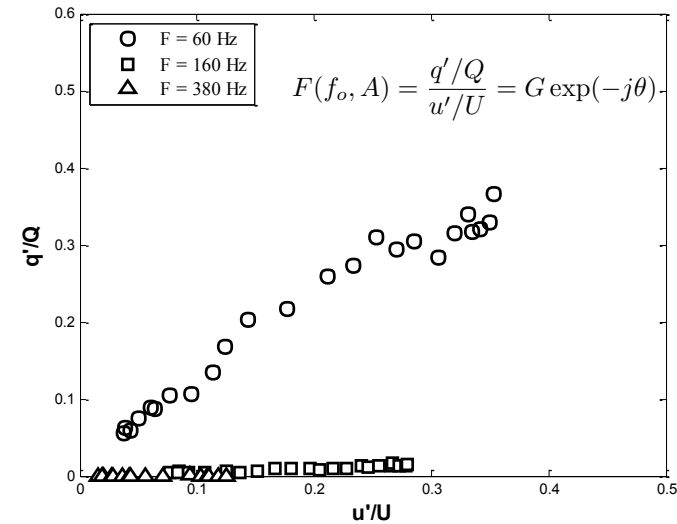
Competing factor dip

Flame behaviour - premixed

- $\Phi_g = 0.60$, $U = 5$ m/s, $SR = 1.0$
 $f_0 = 60$, 160 and 380 Hz



(a) $f_0 = 60$ Hz (b) $f_0 = 160$ Hz (c) $f_0 = 380$ Hz

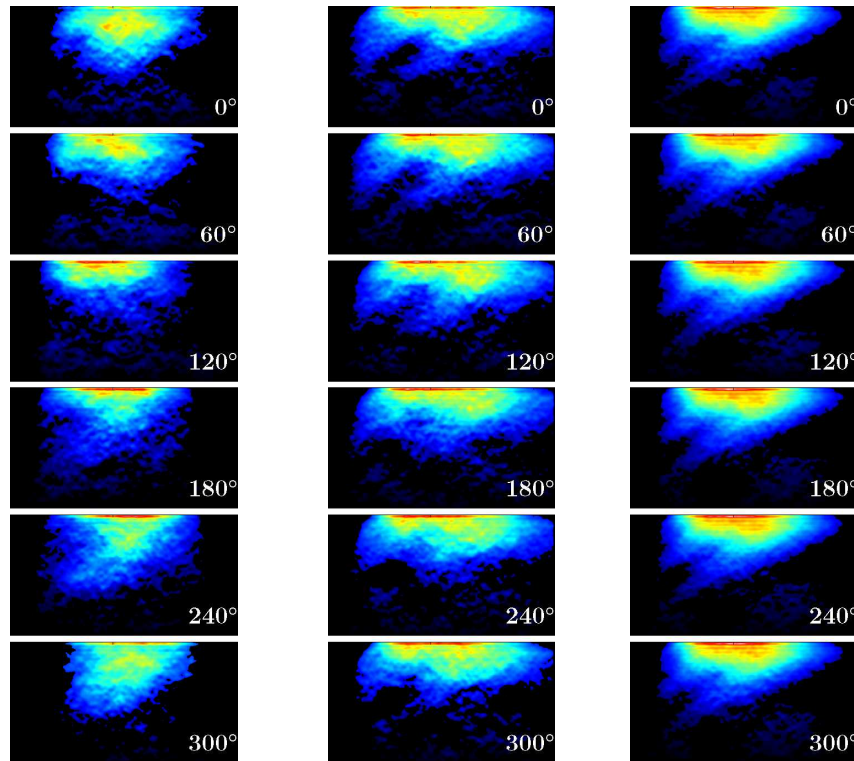


(1) $u'/U = 0.1$
 $f_0 = 60$ Hz

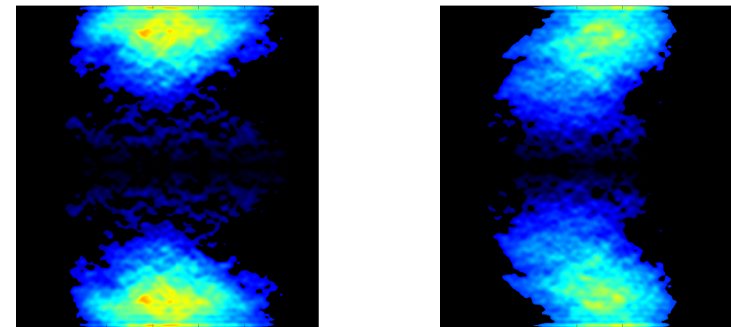
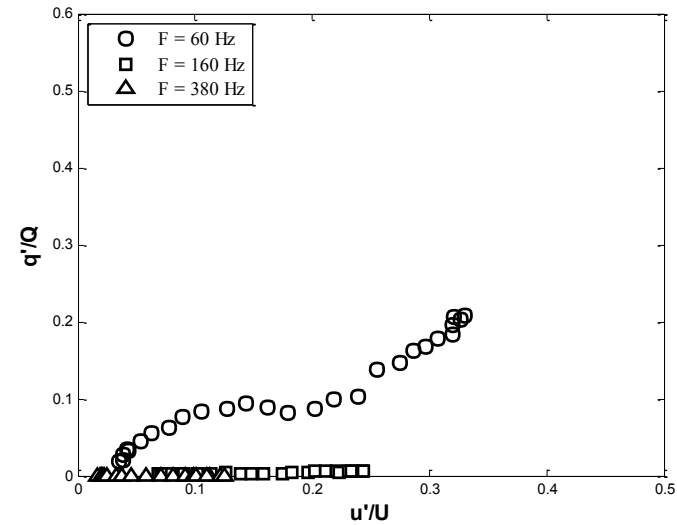
(2) $u'/U = 0.2$

Flame behaviour – SR = 0.5

- $\Phi_g = 0.60$, $U = 5$ m/s, $SR = 0.5$
 $f_0 = 60, 160$ and 380 Hz



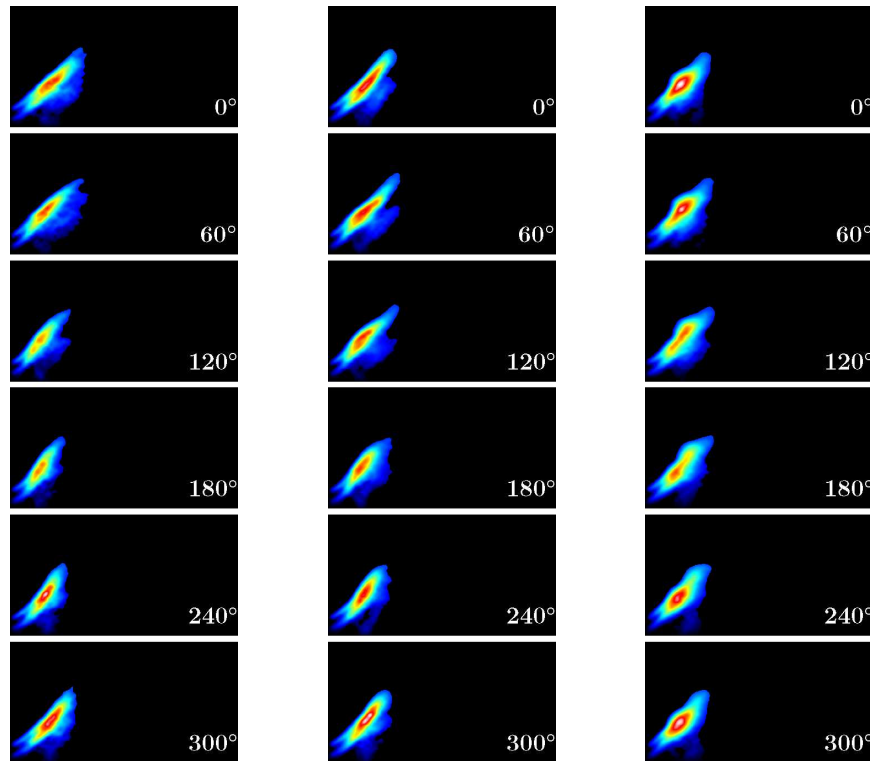
(a) $f_0 = 60$ Hz (b) $f_0 = 160$ Hz (c) $f_0 = 380$ Hz



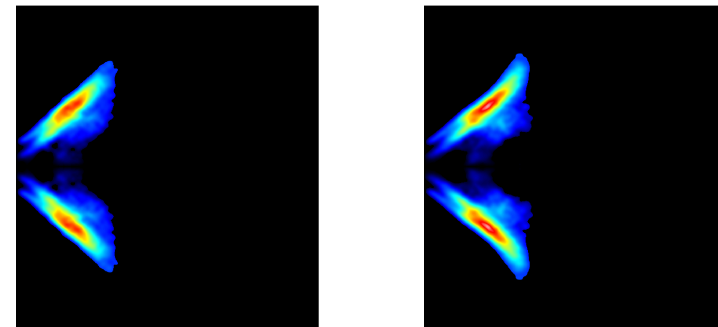
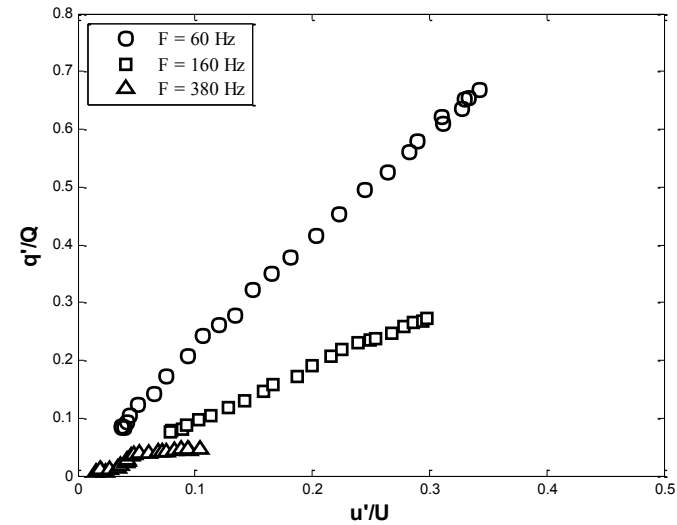
(1) $u'/U = 0.1$
 $f_0 = 60$ Hz (2) $u'/U = 0.2$

Flame behaviour – SR = 2.0

- $\Phi_g = 0.60$, $U = 5$ m/s, $SR = 2.0$
 $f_0 = 60, 160$ and 380 Hz



(a) $f_0 = 60$ Hz (b) $f_0 = 160$ Hz (c) $f_0 = 380$ Hz

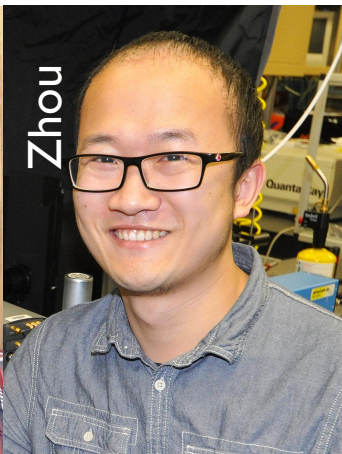
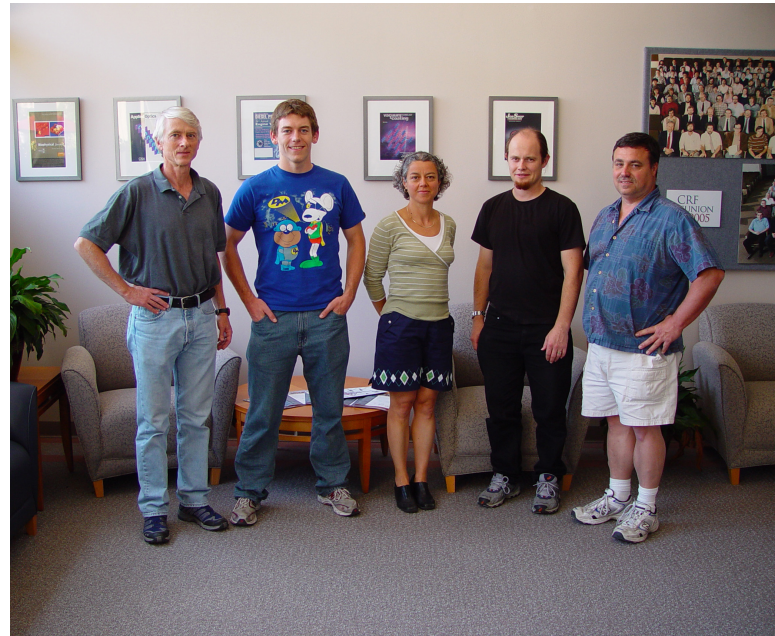


(1) $u'/U = 0.1$
 $f_0 = 60$ Hz

(2) $u'/U = 0.2$

- Effects of fuel distribution on turbulent flame behaviour
 - Macrostructure – large effect, interaction with swirl
 - Microstructure – local stratification *does* affect scalars – should models incorporate the effect?
 - What about NO_x and CO?
 - Effects of fuel distribution on combustion instabilities
 - Location, timing of heat release
 - Sensitivity to acoustic perturbations
 - Small changes, big effects
- ✓ Increased complexity, but great opportunities

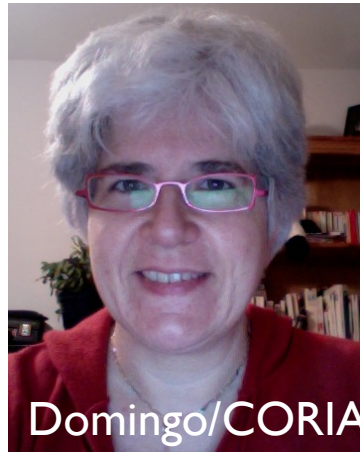
Collaborators



Collaborators – LES Models



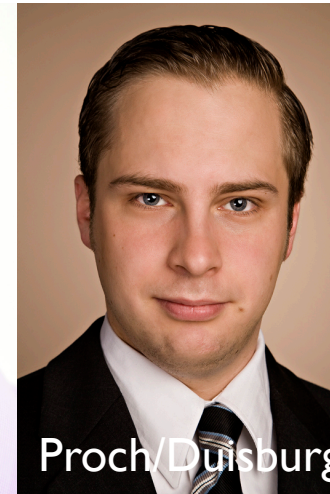
Vervisch/CORIA



Domingo/CORIA



Kempf/Duisburg



Proch/Duisburg



Fiorina/EM2C



Mercier/EM2C



Kuenne/TUD